

The interplay of inertia and elasticity in polymeric flows

Rahul Kumar Singh¹ and Marco Edoardo Rosti¹

¹Complex Fluids and Flows Unit, Okinawa Institute of Science and Technology Graduate University (OIST), 1919-1, Tancha, Onna-son, Okinawa 904-0495, Japan

Corresponding author: Marco Edoardo Rosti, marco.rosti@oist.jp

(Received 7 November 2024; revised 5 June 2025; accepted 22 July 2025)

Addition of polymers modifies a turbulent flow in a manner that depends non-trivially on the interplay of fluid inertia, quantified by the Reynolds number Re , and the elasticity of the dissolved polymers, given by the Deborah number De . We use direct numerical simulations to study polymeric flows at different Re and De numbers, and uncover various features of their dynamics. Polymeric flows exhibit a non-unique scaling of the energy spectrum that is a function of Re and De , owing to different dominant contributions to the total energy flux across scales, with the weakening of fluid nonlinearity with decreasing Re also leading to the reduction of the polymeric scaling range. This behaviour is also manifested in the real space scaling of structure functions. We also shed light on how the addition of polymers results in slowing down the fluid nonlinear cascade resulting in a depleted flux, as velocity fluctuations with less energy persist for longer times in polymeric flows, especially at intermediate Re numbers. These velocity fluctuations exhibit intermittent, large deviations similar to that in a Newtonian flow at large Re , but differ more and more as Re becomes smaller. This observation is further supported by the statistics of fluid energy dissipation in polymeric flows, whose distributions collapse on to the Newtonian at large Re , but increasingly differ from it as Re decreases. We also show that polymer dissipation is significantly less intermittent compared with fluid dissipation, and even less so when elasticity becomes large. Polymers, on an average, dissipate more energy when they are stretched more, which happens in extensional regions of the flow. However, owing to vortex stretching, regions with large rotation rates also correlate with large polymer extensions, albeit to a relatively less degree than extensional regions.

Key words: homogeneous turbulence, turbulence simulation, viscoelasticity

1. Introduction

Polymeric flows are very well known to give rise to a wide range of intriguing phenomena. The pioneering work by Toms (1949) showed that a small concentration of polymers added to a carrier flow results in the reduction of turbulent drag, which was reviewed in Lumley (1973), Virk (1975), Toms (1977) and Berman (1978). Ever since this discovery, there have been numerous theoretical (Tabor & de Gennes 1986; Bhattacharjee & Thirumalai 1991; Sreenivasan & White 2000; L'vov *et al.* 2004; Procaccia, L'vov & Benzi 2008), numerical (Benzi *et al.* 2003; Kalelkar, Govindarajan & Pandit 2005; Perlekar, Mitra & Pandit 2006; Gillissen 2008; White & Mungal 2008; Choueiri, Lopez & Hof 2018; Xi 2019; Rosti, Perlekar & Mitra 2023) and experimental (Den Toonder *et al.* 1997; Escudier, Presti & Smith 1999; Ptasiński *et al.* 2001, 2003; Yang & Dou 2010) works in an attempt to better understand and highlight its origins and the underlying mechanisms. Lumley (1973) and Hinch (1977) showed that dissolved polymers tend to increase the effective viscosity of a solution; however, there can be a net reduction in the dissipation of energy in such turbulent, polymeric flows, as was pointed out by van Doorn *et al.* (1999), Kalelkar *et al.* (2005), Perlekar *et al.* (2006, 2010) and Cai, Li & Zhang (2010). This rich, and complex behaviour of polymeric flows is dictated by an interplay of two intrinsic features: inertia and elasticity. Inertia is a property of the Newtonian, carrier flow, whose strength is determined by the non-dimensional Reynolds number Re . A large Re is typically indicative of a highly turbulent flow where flow structures span a wide range of scales. Elasticity, on the other hand, is a characteristic of the polymers, which determines their tendency to stretch and is quantified by the non-dimensional Deborah number De . A large De means the polymers take longer to relax back to their equilibrium lengths and remain stretched for longer times.

Experiments by Larson (1992), Shaqfeh (1996), Groisman & Steinberg (1998) and Pan *et al.* (2013) have shown that flows at small Re develop instabilities when polymers are added in small concentrations. At extremely small Re , when fluid nonlinearity remains dormant, instabilities driven by purely elastic effects result in a flow state referred to as elastic turbulence (ET) which shows qualitatively similar behaviour to classical high Re turbulence (HIT) in many respects. These include the existence of a chaotic flow state, as illustrated in the works of Groisman & Steinberg (2000, 2004) and Qin & Arratia (2017), as well as enhancement of mixing Groisman & Steinberg (2001) and heat transfer Li *et al.* (2017). A self-similar distribution of kinetic energy over a wide range of scales was also observed in numerical simulations of ET (Berti *et al.* 2008; Berti & Boffetta 2010; Ray & Vincenzi 2016; Gupta & Vincenzi 2019; Soligo & Rosti 2023; Foggi Rota *et al.* 2024; Lewy & Kerswell 2024; Singh *et al.* 2024). At larger, yet moderate Re , it is now known that polymer elasticity and the fluid nonlinearity (albeit with a weaker contribution as shown by Gillissen (2021)) conspire to trigger a turbulence-like behaviour much earlier than that in a Newtonian flow (Dubief, Terrapon & Soria 2013; Samanta *et al.* 2013; Valente, da Silva & Pinho 2016; Dubief, Terrapon & Hof 2023). Such a flow state at moderate Re is referred to as elastoinertial turbulence. Fluid kinetic energy in elastoinertial turbulence is also known to exhibit a distinct self-similar, scaling behaviour (Zhang *et al.* 2021a; Dubief *et al.* 2013; Valente *et al.* 2016). At very large Re numbers, turbulent polymeric flows (PHIT) exhibit a novel self-similar spectrum whose scaling exponents differ from those predicted by the Kolmogorov theory (K41) for classical Newtonian turbulence (i.e. HIT) (Kolmogorov 1941; Frisch 1996). This was uncovered recently in the experiments of Zhang *et al.* (2021b) as well as in the numerical simulations of Rosti *et al.* (2023).

In this work, we study turbulent polymeric flows in a triperiodic box across a wide range of Re and De numbers, and show how various aspects of their dynamics transition when moving from low (Singh *et al.* 2024) to large (Rosti *et al.* 2023) Reynolds number.

We show that the addition of polymers results in a non-unique scaling of the energy spectrum, that emerges as a result of different underlying dominant flux contributions. The fluxes, furthermore, reveal that polymers slow down the rate of energy transfer via the fluid nonlinear cascade, signalling a weakened fluid nonlinear cascade. We then discuss how polymers are, in turn, themselves affected by Newtonian carrier flow. In particular, we show that the polymers stretch in both the extensional and rotational regions of the flow, with the correlation being less for the latter. Both fluid and polymer extensions are directly related to the corresponding dissipations, which show contrasting characteristics. Fluid dissipation shows more large deviations about the mean at small Re and large De , while polymer dissipation is less intermittent, and even lesser at large De . We structure all of the above as follows: the details of numerical simulations are provided in the immediately following § 2 before moving on to the results in § 3. Finally, we summarise our conclusions in § 4.

2. Mathematical model and numerical method

We arrive at our results via the direct numerical simulations of polymeric flows that comprise an incompressible Newtonian carrier fluid whose dynamics is described by a velocity field $\mathbf{u}$ ($\nabla \cdot \mathbf{u} = 0$), with dissolved polymers that are described by a conformation tensor field $\mathbf{C}$. The trace of this conformation field $Tr(\mathbf{C}) = C_{ii}(\mathbf{x}, t)$ (with $i = 1, 2, 3$) is an average measure of the squared end-to-end lengths of the polymers. In particular, we adopt the Oldroyd-B model of polymers, which has often been used to study polymeric flows in various settings in a number of works (Vincenzi *et al.* 2007; Berti *et al.* 2008; Bagheri *et al.* 2012; De Lillo, Boffetta & Musacchio 2012; Gupta & Vincenzi 2019; Zhang *et al.* 2021a; Rosti *et al.* 2023; Aswathy & Rosti 2024). The flow is described by the simultaneous evolution of the coupled equations,

$$\rho (\partial_t \mathbf{u} + \mathbf{u} \cdot \nabla \mathbf{u}) = -\nabla p + \mu_s \nabla^2 \mathbf{u} + \frac{\mu_p}{\tau_p} \nabla \cdot \mathbf{C} + \mathbf{F}, \quad (2.1a)$$

$$\partial_t \mathbf{C} + \mathbf{u} \cdot \nabla \mathbf{C} = \mathbf{C} \nabla \mathbf{u} + (\nabla \mathbf{u})^T \mathbf{C} - \frac{1}{\tau_p} (\mathbf{C} - \mathbf{I}), \quad (2.1b)$$

where ρ is the fluid density, p the pressure, μ_s the dynamic viscosity of the Newtonian fluid (kinematic viscosity $\nu = \mu_s/\rho$), μ_p the dynamic polymer viscosity and τ_p is the unique relaxation time of the polymers. A statistically stationary state is maintained by energy injection via the forcing $\mathbf{F}$ for which we employ the *ABC* scheme such that $\mathbf{F} = \nu[(A \sin z + C \cos y) \hat{x} + (B \sin x + A \cos z) \hat{y} + (C \sin y + B \cos x) \hat{z}]$, where $A = B = C = 1$. The total energy injected per unit time ϵ_t is dissipated away by both the Newtonian fluid (ϵ_f) and the polymers (ϵ_p), such that $\epsilon_t = \epsilon_f + \epsilon_p$.

The flow is characterised by two dimensionless numbers: the Taylor-scale Reynolds number, $Re_\lambda \equiv u_{rms} \lambda / \nu$, where $\lambda \equiv u_{rms} \sqrt{15 \nu / \epsilon_f}$ is the Taylor length scale and u_{rms} the root mean square velocity, and the Deborah number, $De \equiv \tau_p / \tau_L$, where $\tau_L = L / u_{rms}$ is the large-eddy turnover time, with $L = 2\pi$ being the scale of the forcing. We vary Re_λ in the range between 40 and 450 and $De \in \{1/9, 1/3, 1, 3, 9\}$. Lastly, we fix fluid and polymer viscosities such that $\mu_s / (\mu_s + \mu_p) = 0.9$. All cases considered in this work are listed in table 1; note that, the last six simulations with $Re_\lambda \approx 40$ are the same presented by Singh *et al.* (2024), while the first six are similar to those discussed by Rosti *et al.* (2023), but repeated here with a different forcing scheme for the sake of consistency with the rest of the study. All the 10 intermediate cases are completely novel, and represent the heart of the present investigation.

Re_λ	De	u_{rms}	ϵ_f	ϵ_p	Ω	η	τ_L
450	—	6.6	63.0	—	2.8×10^4	3.7×10^{-3}	9.5×10^{-1}
470	1/9	6.5	54.1	8.4	2.4×10^4	3.8×10^{-3}	9.7×10^{-1}
583	1/3	7.0	45.8	25.0	2.0×10^4	4.0×10^{-3}	9.0×10^{-1}
816	1	6.4	17.1	50.2	7.6×10^3	5.1×10^{-3}	9.8×10^{-1}
713	3	5.8	14.5	44.2	6.4×10^3	5.3×10^{-3}	1.1×10^0
772	9	6.3	17.4	52.7	7.7×10^3	5.1×10^{-3}	1.0×10^0
317	—	8.0	60.9	—	1.4×10^4	6.2×10^{-3}	9.6×10^{-1}
510	1	7.4	16.7	48.2	3.7×10^3	8.6×10^{-3}	1.0×10^0
240	—	7.3	83.8	—	9.3×10^3	9.7×10^{-3}	8.6×10^{-1}
250	1/9	6.9	61.2	12.5	6.8×10^3	1.0×10^{-2}	9.1×10^{-1}
293	1/3	6.1	26.5	30.7	2.9×10^3	1.3×10^{-2}	1.0×10^0
316	1	5.5	15.4	42.6	1.7×10^3	1.5×10^{-2}	1.1×10^0
312	3	6.3	26.7	52.5	3.0×10^3	1.3×10^{-2}	1.0×10^0
240	9	5.5	27.0	44.3	3.0×10^3	1.3×10^{-2}	1.1×10^0
103	—	6.2	58.4	—	1.6×10^3	3.0×10^{-2}	1.0×10^0
166	1	6.1	20.3	49.3	5.6×10^2	3.9×10^{-2}	1.0×10^0
42	—	6.0	60.9	—	2.3×10^2	9.9×10^{-2}	1.0×10^0
56	1/9	6.5	49.2	50.5	2.7×10^2	1.0×10^{-1}	1.0×10^0
39	1/3	5.2	39.1	62.3	2.2×10^2	1.1×10^{-1}	1.2×10^0
49	1	5.5	31.2	44.7	1.7×10^2	1.2×10^{-1}	1.1×10^0
34	3	4.4	25.5	33.9	1.4×10^2	1.2×10^{-1}	1.4×10^0
32	9	4.4	30.2	26.8	1.7×10^2	1.2×10^{-1}	1.4×10^0

Table 1. Details of the numerical simulations considered in the present study. Here De is the Deborah number, Re_λ is the Reynolds number based on u_{rms} and on the Taylor length scale λ , ϵ_f , ϵ_p are the mean fluid and polymer dissipation of energy, Ω is the mean enstrophy, η is the Kolmogorov length scale and τ_L is the large eddy turnover time scale of the flow.

We solve the fluid velocity and polymer conformation tensor field given by (2.1a) and (2.1b) on a staggered, uniform, Cartesian grid, using the in-house flow solver [Fujin](#), which employs a second-order central finite difference scheme for spatial discretisation. Time marching is achieved via a second-order Adams–Bashforth scheme coupled with a fractional step method (Kim & Moin 1985), except for the non-Newtonian stress term which is advanced in time via the Crank–Nicolson scheme. In the momentum equation we use the Adams–Bashforth scheme for time advancement for all terms except for the polymer contribution, because this can be advanced implicitly with the Crank–Nicolson scheme, since its updated value is found separately from the additional transport equation. In the polymeric equation, we still use the second-order Adams–Bashforth scheme for all terms, except for the advection term for which we use the high-order weighted essentially non-oscillatory scheme (Sugiyama *et al.* 2011) scheme. A log-conformation formulation is also used for (2.1b), to ensure positive-definiteness of the conformation tensor at all times (see Izbassarov *et al.* 2018). Indeed, all these schemes, together with the use of the log conformation formulation for the polymeric equation, allows to overcome the notorious high Deborah numerical instability (Min, Yoo & Choi 2001), without any explicit artificial diffusion term, as discussed in previous papers (see e.g. Min *et al.* 2001; Sugiyama *et al.* 2011; Izbassarov *et al.* 2018). Obtaining incompressible fluid velocity at each time requires solving a Poisson equation for pressure, which is done using a solver based on the fast Fourier transform. The solver is parallelised using the domain decomposition library [2decomp](#) and the MPI protocol.

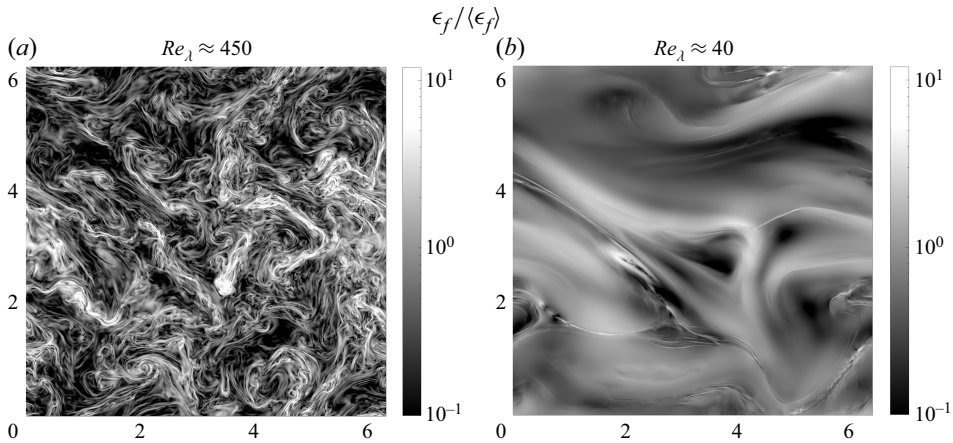


Figure 1. Representative snapshots of normalised fluid energy dissipation rates ϵ_f at (a) large and (b) small Re for $De \approx 1$. Large Re_λ polymeric flows exhibit a wide range of flow structures, while the small Re_λ flows have only large-scale structures.

We solve (2.1) on a $2\pi \times 2\pi \times 2\pi$ -periodic domain that is discretised into $N^3 = 1024^3$ points. The smallest spatial scales resolved are equal to 0.05η and η for the smallest and largest Re_λ simulations. We choose two different time steppings of $\delta t = 1.25 \times 10^{-5}$ and $\delta t = 2.5 \times 10^{-5}$ for small and large Re_λ simulations, which, respectively, equal $1.5 \times 10^{-3}\tau_\eta$ and $2 \times 10^{-3}\tau_\eta$, where τ_η is the Kolmogorov time scale. Field data is saved every 2×10^4 time steps in a stationary state for data analysis with the overall data spanning $\approx 6\tau_L$ for all cases. This means simulating around $54\tau_p$ for the smallest $De = 1/9$, $6\tau_p$ for $De = 1$ and $2\tau_p$ for the largest $De = 9$. We have checked by splitting the data set into half for the largest De that the statistics remain unchanged. We show representative, two-dimensional slices of the dissipation fields ϵ_f for very large and small Re in figure 1 while some typical averaged statistical estimates for the simulations are provided in table 1.

3. Results

3.1. The energy spectra

We begin our study by investigating how energy is distributed across scales in a statistically stationary state in flows of polymeric fluids. The distribution of energy is given by its spectrum $E(k)$ which is a measure of the energy content at scale (mode) k such that the total energy $\mathcal{E} = \langle |\mathbf{u}|^2 \rangle / 2 = \int E(k) dk$. The energy spectrum is one of the most commonly studied quantities in turbulence and was shown by Kolmogorov (1941) to have a self-similar distribution across scales in (the inertial range of) HIT as $E(k) \sim k^{-5/3}$ (see also Frisch 1996). We now show in figure 2 how this self-similar distribution of fluid kinetic energy is modified in PHIT, and its dependence on polymer elasticity De in figure 2(a) and the intensity of turbulence Re_λ in figure 2(b).

Figure 2(a) shows how the spectrum $E(k)$ changes with De at large $Re_\lambda \approx 450$. When De is small, i.e. in the limit $\tau_p \rightarrow 0$, polymers are stretch minimally, and remain close to their equilibrium unstretched configuration $\mathbf{C} \approx \mathbf{I}$. This is easily seen by multiplying (2.1b) by τ_p , and taking the limit $\tau_p \rightarrow 0$,

$$\tau_p (\partial_t \mathbf{C} + \mathbf{u} \cdot \nabla \mathbf{C}) = \tau_p (\mathbf{C} \nabla \mathbf{u} + (\nabla \mathbf{u})^T \mathbf{C}) - (\mathbf{C} - \mathbf{I}) \xrightarrow{\tau_p \rightarrow 0} \mathbf{C} - \mathbf{I} = 0. \quad (3.1)$$

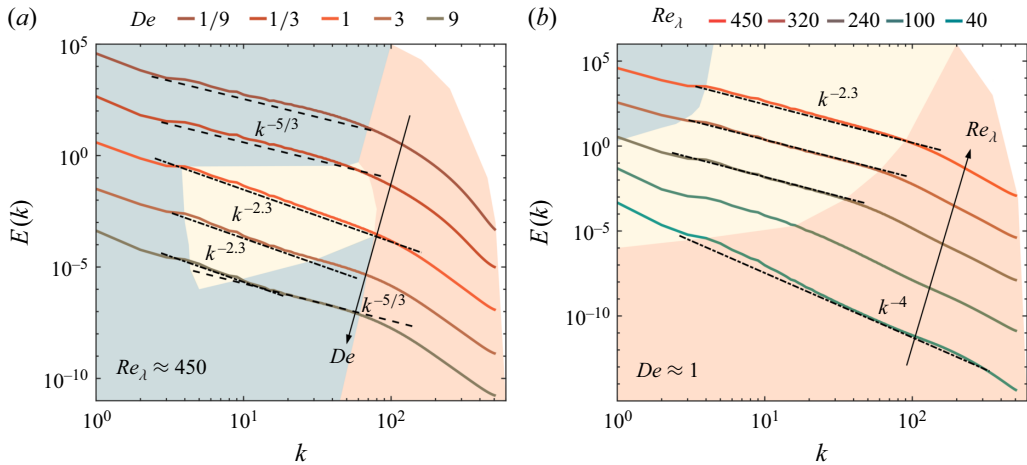


Figure 2. The non-unique scaling of the fluid energy spectrum $E(k)$ in polymeric flows at different (a) De and (b) Re_λ numbers. The spectra have been shifted vertically for visual clarity by factors of powers of 10. Three distinct scaling regimes (in different shades) have been shown in dashed ($k^{-5/3}$, Newtonian), dash-dotted ($k^{-2.3}$, polymeric) and dotted ($k^{-\gamma}$; $\gamma \geq 4$, smooth) lines. All three regimes coexist when $De \approx 1$. (a) The smallest De has a close to Newtonian behaviour as the elastic effects are minimal. (b) The triple scaling at largest Re gives way to a unique, smooth k^{-4} regime at the smallest Re_λ .

As the fluctuations in $\mathbf{C}$ are small, the polymer stresses in (2.1a) have a minimal contribution: $\nabla \cdot \mathbf{C} \approx 0$. Thus, elastic effects do not play a significant role at small De , and the behaviour remains largely Newtonian. This results in the classical K41, Newtonian-like scaling $E(k) \sim k^{-5/3}$ in figure 2(a). (Henceforth, we refer to this classical scaling range as the Newtonian regime.) This intermediate, Newtonian scaling range is of course followed by the dissipation range where the spectrum shows an exponential decay, a consequence of velocity fields being analytic.

As De is increased, polymers begin to stretch to longer lengths so that $\mathbf{C}$ now ventures far from $\mathbf{I}$ and has rather large spatiotemporal fluctuations. The resulting stretching and relaxation of polymers generates large non-Newtonian stresses (given by $(\mu_p/\tau_p)\nabla \cdot \mathbf{C}$) on the carrier fluid, especially for a large enough elasticity as $De \approx 1$. The resulting dominant elastic effects along with a suppressed fluid nonlinearity (see § 3.2 for detailed discussion) means that the energy spectrum is modified to $E(k) \sim k^{-2.3}$ at large Re_λ , as was also observed by Zhang *et al.* (2021a) and Rosti *et al.* (2023). (We refer to this as the polymeric range, henceforth.) Viscous effects begin to dominate beyond this polymeric range and the fluid nonlinearity ceases to have any contribution. The polymeric stresses, however, are still active in this range due to the small scale fluctuations in polymer lengths which, in turn, create fluctuations in the fluid velocity. Consequently, the spectrum exhibits a steep power-law decay $E(k) \sim k^{-\delta}$ with $\delta \geq 4$, rather than an exponential fall-off in the smooth dissipative range. Thus, the elasticity of polymers results in a dual scaling behaviour of the energy spectrum $E(k) \sim k^{-\delta}$ in PHIT, especially for $De \approx 1$ (see figure 2a), with the exponent $\delta \approx 2.3$ in the intermediate, polymeric range of scales ($6 \lesssim k \lesssim 60$) and $\delta \gtrsim 4$ for $k \gtrsim 100$ in the smooth but steep dissipative range.

On a further increase in polymer elasticity, the back reaction of polymers on the Newtonian carrier flow begins to diminish. This is because polymers with very large relaxation times respond to the background flow after a large time lag, thereby staying in a stretched configuration for long times. This means fluctuations in polymer lengths are suppressed at large De as polymer lengths do not change appreciably in space. As a result,

their gradients also remain typically small thereby weakening the elastic stresses $\nabla \cdot \mathbf{C}$ on an average. This is coupled with the fact that a large factor of τ_p further weakens the feedback of polymer stresses on the carrier flow. Thus, Newtonian scaling is recovered for large De , and is seen in the re-emergence of $E(k) \sim k^{-5/3}$ regime at $De \approx 9$. Indeed, at even larger De we have an intermediate range of scales with completely Newtonian scaling behaviour Rosti *et al.* (2023). Again in the deep dissipation range, small fluctuations in the polymer lengths result in fluctuations of the flow field, which are rough at the subleading order with a steep power-law decay of the spectrum as $E(k) \sim k^{-4}$.

Figure 2(b) shows the dependence of the energy spectrum on Re_λ , where we plot $E(k)$ for a fixed polymer elasticity of $De \approx 1$. The top curve is just the spectrum at $Re_\lambda \approx 450$ and $De \approx 1$. Now, it is well known that with decreasing Re_λ in HIT the fluid nonlinearity becomes increasingly less important (with respect to viscous dissipation) causing the inertial range to shrink (and the viscous dissipation range to widen). In PHIT, a decreasing Re_λ entails that now the intermediate polymeric range shrinks as seen from figure 2(b). This is a consequence of the fluid inertia weakening even further in the presence of polymers (see § 3.2 for detailed discussion). A further weakened fluid inertia means that viscosity becomes important at even larger scales. The dissipative range thus widens, and the steep power-law fall-off begins at even smaller k as Re_λ decreases. In fact, at $Re_\lambda \approx 40$, the polymeric regime is completely absent and the smooth dissipation range spans the entire range of scales (see also Singh *et al.* 2024). This is indeed very different from Newtonian turbulence, where a decreasing Re_λ results in a shrinking inertial range that completely disappears as $Re_\lambda \rightarrow 0$ and the spectrum decays exponentially. Polymeric turbulence, on the other hand, shows a transition from $E(k) \sim k^{-2.3}$, as Re_λ decreases, to a steeper power-law spectrum of $E(k) \sim k^{-4}$ as $Re_\lambda \rightarrow 0$ for large De .

Next, we discuss how different dominant contributions lead to this non-unique scaling behaviour in polymeric flows, as a function of Re_λ and De .

3.2. The flux contributions

The coexistence of various scaling regimes of the energy spectrum, as discussed in § 3.1, can be better understood by looking at the dominant energy transfer mechanisms across scales (see also Casciola & De Angelis (2007) for a similar discussion on spectral decomposition with a slightly different approach). We obtain these dominant contributions from (2.1a) by computing its Fourier transform and its complex conjugate,

$$\partial_t \hat{u}_i(\mathbf{k}) + \mathcal{N}_i(\mathbf{k}) = ik_i \hat{p} - \nu k^2 \hat{u}_i(\mathbf{k}) + \frac{\mu_p}{\rho \tau_p} ik_j \hat{C}_{ij} + \hat{F}_i(\mathbf{k}), \quad k_i \hat{u}_i = 0; \quad (3.2a)$$

$$\partial_t \hat{u}_i^\dagger(\mathbf{k}) + \mathcal{N}_i^\dagger(\mathbf{k}) = -ik_i \hat{p}^\dagger - \nu k^2 \hat{u}_i^\dagger(\mathbf{k}) - \frac{\mu_p}{\rho \tau_p} ik_j \hat{C}_{ij}^\dagger + \hat{F}_i^\dagger(\mathbf{k}), \quad (3.2b)$$

where the hat $\hat{\cdot}$ denotes the Fourier transformed variables, $\cdot^\dagger$ denotes the complex conjugate and $\mathcal{N}_i(\mathbf{k})$ is the Fourier transform of the fluid nonlinear term. Summation over repeated indices is implied. The energy equation for any k th mode can be obtained by multiplying (3.2a) by $\hat{u}_i^\dagger(\mathbf{k})$, and (3.2b) by $\hat{u}_i(\mathbf{k})$, and adding the two together,

$$\partial_t \mathcal{E}(\mathbf{k}) + \text{Re}(\hat{u}_i^\dagger(\mathbf{k}) \mathcal{N}_i(\mathbf{k})) = -2\nu k^2 \mathcal{E}(\mathbf{k}) + \frac{\mu_p}{\rho \tau_p} \text{Im}(\hat{u}_i^\dagger(\mathbf{k}) k_j \hat{C}_{ij}) + \text{Re}(\hat{u}_i^\dagger(\mathbf{k}) \hat{F}_i(\mathbf{k})), \quad (3.3)$$

where $\mathcal{E}(\mathbf{k}) = |\hat{u}_i(\mathbf{k})|^2/2$ is the energy in mode $\mathbf{k}$, the pressure term vanishes away due to incompressibility, and $\text{Re}(\cdot)$ and $\text{Im}(\cdot)$ denote the real and imaginary parts, respectively. The total energy flux from modes $k < K$ to those $k > K$ can be obtained by integrating

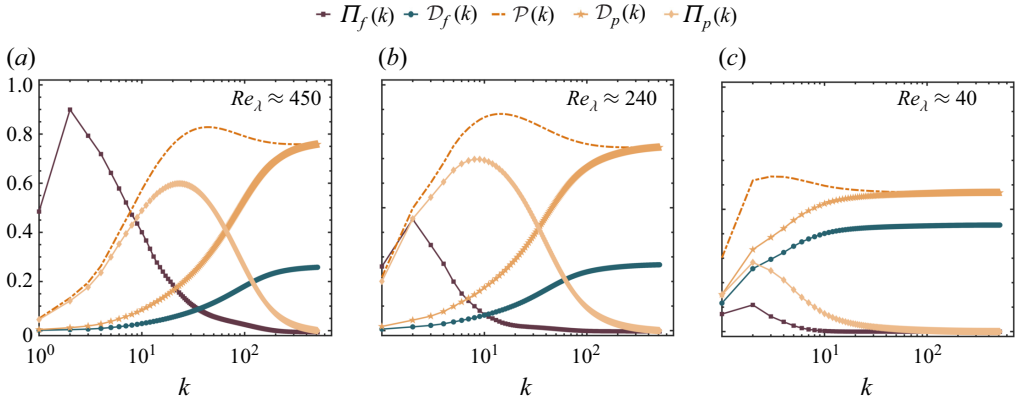


Figure 3. Normalised flux contributions at (a) $Re_\lambda \approx 450$, (b) 240 and (c) 40 for flows with $De \approx 1$. The polymeric contribution $\mathcal{P}$ is split into flux Π_p and dissipation $\mathcal{D}_p$ contributions as $\mathcal{P} = \Pi_p + \mathcal{D}_p$ as in Rosti *et al.* (2023). (a) At large Re_λ , three distinct regimes are determined by different dominant contributions: large scales are dominated by the fluid nonlinear flux Π_f ; intermediate scales by the polymer flux Π_p ; small scales by the polymer dissipation $\mathcal{D}_p$. (b) At moderate Re_λ , the fluid-nonlinearity Π_f is weakened and comprises two distinct regimes dominated by Π_p and $\mathcal{D}_p$. (c) At extremely small Re_λ , only the dissipative terms $\mathcal{D}_f$, $\mathcal{D}_p$ remain important. All terms are normalised by ϵ_t .

from 0 to K ,

$$\begin{aligned} \partial_t \int_0^K d\mathbf{k} \mathcal{E}(\mathbf{k}) + \int_0^K d\mathbf{k} \operatorname{Re} (\hat{u}_i^\dagger(\mathbf{k}) \mathcal{N}_i(\mathbf{k})) = \\ -\nu \int_0^K d\mathbf{k} k^2 |\hat{u}_i(\mathbf{k})|^2 + \frac{\mu_p}{\rho \tau_p} \int_0^K d\mathbf{k} \operatorname{Im} (\hat{u}_i^\dagger(\mathbf{k}) k_j \hat{C}_{ij}) + \int_0^K d\mathbf{k} \operatorname{Re} (\hat{u}_i^\dagger(\mathbf{k}) \hat{F}_i(\mathbf{k})). \end{aligned} \quad (3.4)$$

In a statistically stationary state, the total energy in any set of modes is a constant, so that $\partial_t \int_0^K d\mathbf{k} \mathcal{E}(\mathbf{k}) = 0$. Choosing suitable symbols for the remaining integrals, and using isotropy to argue that their dependence is only on $K = |\mathbf{K}|$, we have

$$\Pi'_f(K) = -\mathcal{D}'_f(K) - \mathcal{P}'(K) + \mathcal{F}(K), \quad (3.5)$$

where Π'_f , $\mathcal{D}'_f$, $\mathcal{P}'$ and $\mathcal{F}$ are the contributions from fluid nonlinearity, fluid dissipation, polymer stresses and the external forcing, respectively. Since the forcing $\hat{F}_i$ is applied at only $K = 1$, we have that $\mathcal{F}(K)$ is a constant for any $K > 1$,

$$\Pi'_f(K) + \mathcal{D}'_f(K) + \mathcal{P}'(K) = \mathcal{F}(K) = \epsilon_t, \quad (3.6)$$

where ϵ_t is the rate of total energy injection into the system by the forcing $\mathbf{F}$. Thus, upon normalisation by ϵ_t , we obtain

$$\Pi_f(K) + \mathcal{D}_f(K) + \mathcal{P}(K) = 1, \quad (3.7)$$

where $\Pi_f = \Pi'_f/\epsilon_t$, $\mathcal{D}_f = \mathcal{D}'_f/\epsilon_t$, $\mathcal{P} = \mathcal{P}'/\epsilon_t$ (see also Abdelgawad, Cannon & Rosti 2023). We show the curves for all the three contributions, Π_f , $\mathcal{D}_f$ and $\mathcal{P}$, as a function of Re_λ in figure 3, for a polymer elasticity of $De \approx 1$. Following Rosti *et al.* (2023), we partition the polymeric contribution into flux (Π_p) and dissipative ($\mathcal{D}_p$) terms as

$$\mathcal{P}(K) = \Pi_p(K) + \mathcal{D}_p(K), \quad \text{where} \quad \mathcal{D}_p(K) \equiv (\epsilon_p/\epsilon_f) \mathcal{D}_f(K). \quad (3.8)$$

Such a definition is motivated by the requirement that at small scales (or large k) the polymeric term must get all its contribution from dissipative effects. Indeed, the full

polymeric contribution $\mathcal{P}$ captures both the dissipative and flux contributions. We note that a purely dissipative part $\mathcal{D}_p$ of $\mathcal{P}$ must be monotonically growing in k , thus we choose to model $\mathcal{D}_p$ in the very simple and naïve way by prescribing the same scale dependence as the fluid dissipation $\mathcal{D}_f$, which we already know grows monotonically in k . We tried different prescriptions for $\mathcal{D}_p$ under the constraint of $\mathcal{D}_p = 0$ at $k = 0$, $\mathcal{D}_p = \epsilon_p$ at $k = k_{\max}$ with a monotonic growth. The results do not change qualitatively but only quantitatively, in the sense that the boundaries of the different scaling ranges shift only marginally. Since these changes remain limited, the estimates for where different flux contributions crossover is reasonably robust. We plot the contributions Π_p and $\mathcal{D}_p$ thus obtained in figure 3.

At large Re_λ , figure 3(a) shows that the fluid nonlinearity Π_f has the dominant contribution to the total energy balance at large scales (i.e. for $k \leq 4$). This gives the Newtonian $k^{-5/3}$ scaling at the large but slim band of scales in figure 2. Away from this range, i.e. for $k \gtrsim 10$, the polymeric flux contribution Π_p begins to dominate. This dominant non-Newtonian flux results in a polymeric scaling regime with $E(k) \sim k^{-2.3}$ up to $k \approx 70$ in figure 2 (see also Rosti *et al.* 2023). At yet smaller scales, i.e. for $k \gtrsim 200$, fluid ($\mathcal{D}_f$) and polymer ($\mathcal{D}_p$) dissipation remove energy from the flow rapidly. The polymer contribution Π_p , has a small, subdominant yet non-zero contribution in this range. (This aligns with our assertion of small-scale fluctuations in polymer lengths in § 3.1.) This subdominant contribution results in a fluid velocity spectrum given by a steep power-law decay at large k , in a manner similar to that in ET at very small Re_λ (see Singh *et al.* 2024). Now, as Re_λ is decreased to a moderate value of $Re_\lambda \approx 240$, the fluid nonlinearity is weakened evidently further as seen in figure 3(b), and the flux of energy is primarily via the fluid–polymer interactions Π_p . However, this range is rather limited as a smaller Re_λ also means that viscous effects become important at relatively smaller k . Thus, we have a restricted polymeric and a wider k^{-4} regime at $Re_\lambda \approx 240$ in figure 2(b). Finally, for very small $Re_\lambda \approx 40$ in figure 3(c), $\mathcal{D}_p$ and $\mathcal{D}_f$ are always large while Π_f and Π_p remain subdominant. In fact, Π_f at such small Re_λ is expected to be dormant and indeed shows an exponential fall off in wavenumbers k in figure 4(c). Here Π_p instead decays only as a steep power-law, and forces fluctuations in the velocity field that result in the steep, and extended k^{-4} range in figure 2(d).

3.3. Slowing down the energy cascade

While the above discussion in § 3.1 on flux contributions sheds light on the non-unique scaling nature of the energy spectra, there is more that remains in hiding in figure 3. We uncover this by plotting the flux contributions on a log–log scale in figure 4 which clearly reveals the k -dependence of the flux contributions. We are particularly interested in the fluid Π_f and polymeric Π_p fluxes.

Figure 4(a) shows that at large Re_λ our polymeric regime $E(k) \sim k^{-2.3}$ is marked by a fluid nonlinear flux decaying as $\Pi_f \sim k^{-1.2}$, while Π_p remains almost constant. Now, $E(k)$ and Π_f can be related to each other using the following simple arguments. Here Π_f is the average rate of net energy transfer through a scale k . This means velocity fluctuations u_k up to the scale k transfer their energy to smaller scales in some characteristic time $\tau_k \sim (ku_k)^{-1}$. In HIT, this characteristic time scale is equal to the typical lifetime of an eddy within the K41 phenomenology. This is because energy flux $\Pi_{f,N}$ in the inertial range is a constant, i.e. $\Pi_{f,N} = \epsilon$, with ϵ being the average rate of energy dissipation. Therefore, we have

$$\Pi_{f,N} \sim \frac{u_k^2}{\tau_k} \sim ku_k^3 \sim \epsilon \implies u_k \sim k^{-1/3} \quad (3.9)$$

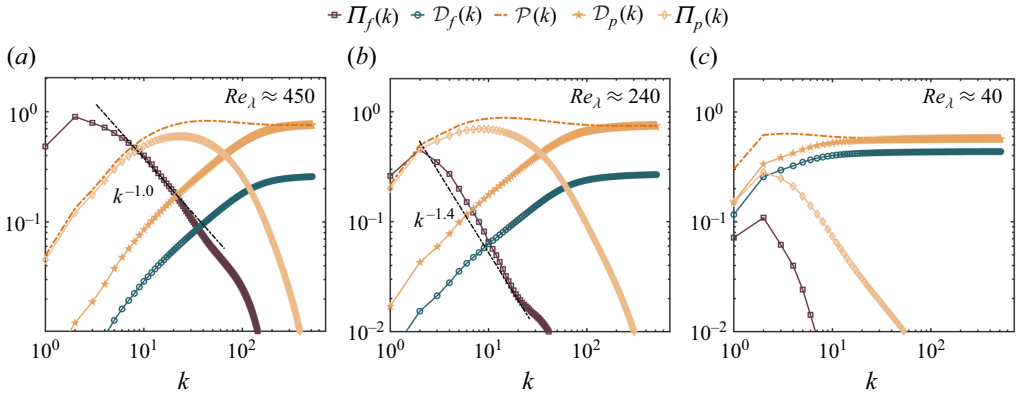


Figure 4. The scaling behaviour of flux contributions obtained by replotting figure 3 on a log–log scale. The approximate scaling forms are shown as dash–dotted lines. The fluid flux Π_f decays as a power-law in the presence of polymers at large to moderate Re_λ , implying a slow and weak fluid nonlinear cascade.

in the inertial range of scales. This means that the time to transfer energy to smaller scales and the typical lifetime of eddies are, respectively, estimated as

$$\tau_{k,N} \sim \frac{u_k^2}{\Pi_{f,N}} \sim \frac{k E_k}{k^0} \sim k^{-2/3}; \quad \tau_{k,N} \sim (k u_k)^{-1} \sim (k k^{-1/3})^{-1} \sim k^{-2/3}. \quad (3.10)$$

In HIT, these time scales are identical as they both are a consequence of a constant inertial range energy flux $\Pi_{f,N}$. This, however, is no longer true in PHIT where the fluid nonlinear flux Π_f is no longer a constant, but is rather a function of the scale k (and therefore is no longer the invariant that determines the scaling form of the velocity fluctuations). For the remainder of this section, we refer to $De = 1$ as it shows maximal deviation from a Newtonian behaviour. We can still estimate the eddy turnover time scale in PHIT as

$$\tau_k \sim (k u_k)^{-1} \sim \left(k \sqrt{k E_k} \right)^{-1} \sim k^{-0.3}. \quad (3.11)$$

So, the typical lifetimes of fluctuations in polymeric turbulence are larger compared with those in Newtonian turbulent flows as τ_k now falls off slower with k . Thus, energy is transferred at a slower rate to smaller scales of the fluid in the presence of polymers. With this knowledge, we can now determine the fate of the fluid nonlinear flux Π_f via the relation $\tau_k \sim u_k^2 / \Pi_f$ as

$$\Pi_f \sim \frac{u_k^2}{\tau_k} \sim \frac{k E_k}{k^{-0.3}} \sim k^{-1.0}. \quad (3.12)$$

Clearly, the scale-by-scale energy transfer via the nonlinear cascade is weakened in polymeric turbulence by the virtue of a smaller proportion of the (total averaged) fluid kinetic energy $u_k^2 / u^2 \sim k^{-1.3}$ being passed onto the larger k at a smaller rate $\tau_k / \tau_L \sim k^{-0.3}$, compared with a Newtonian fluid. The estimated scaling behaviour of $\Pi_f \sim k^{-1}$ is indeed found to hold in figure 4 for the range $k \in [8, 40]$ which is separated from both the forcing effects (acting at $k = 1$) and fluid dissipation (which becomes dominant around $k \approx 40$). (Recall, however, that the energy spectrum scaling $E(k) \sim k^{-2.3}$ holds for the range $k \in [4, 40]$.) This depleted fluid nonlinear flux is accompanied by a finite rate of energy transfer to the dissolved polymers. The typical time scale of this transfer can be estimated by making a crude assumption of a constant polymeric flux, i.e. $\Pi_p \approx k^0$, in $k \in [10, 70]$ from figure 4(a). This assumption then yields

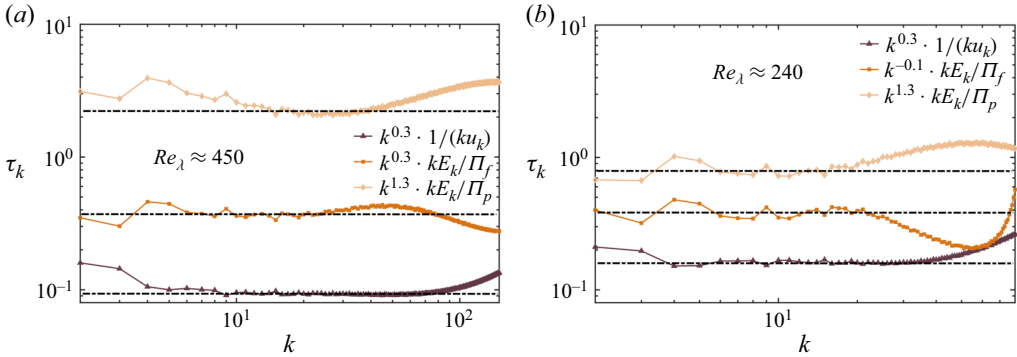


Figure 5. The plots of various time scales discussed in § 3.3 for (a) $Re_\lambda = 450$ and (b) 240, at $De = 1$. We show the compensated plots for the eddy turnover time (triangles) and the time obtained from the nonlinear (squares) and polymer fluxes.

the scale-by-scale energy transfer rate to polymers as

$$\tau_k \sim \frac{u_k^2}{\Pi_p} \sim \frac{kE_k}{k^0} \sim k^{-1.3}. \quad (3.13)$$

This shows that the remaining energy of fluctuations, that was not handed down to the smaller active scales of motion of the carrier fluid by the nonlinear flux, is transferred to the polymers, on an average, at a much faster rate $\tau_k \sim k^{-1.3}$. Now, we expect this relation to hold only approximately for a restricted range of $k \in [10, 40]$ as Π_p is not exactly constant in this range. With these caveats in mind, we now plot the compensated time scales in figure 5(a) for $Re_\lambda = 450$. The relevant ranges are marked by the flattening of the curves which are computed using the relations (3.11), (3.12) and (3.13). Of these, the first two are the estimates of eddy-turnover times/lifetime of velocity fluctuations in polymeric turbulence. Now, the relations (3.11) and (3.12) must yield the same estimates of τ_k up to some constant of $O(1)$. (To obtain τ_k from the second relation (3.12) we use the estimate $\Pi_f \sim k^{-1}$). This is indeed found to be consistent in figure 5(a) where we show these two estimates as curves with triangle and square markers, respectively. And while these curves do not stay flat over a wide range, it is certainly true for the expected range $k \in [8, 40]$. Lastly, the typical time scales of energy transfer to the polymeric mode is given by the compensated curve in diamond markers which corresponds to the relation (3.13). In confirmation to our expectations, we indeed find that this curve is (approximately) flat in the range $k \in [10, 40]$ in figure 4(a). So, it is indeed the case that polymers extract energy at a faster rate from turbulence than the fluid nonlinearity transfers the remaining to smaller scales, on an average resulting in a weakened cascade/fluid nonlinearity.

We now turn our attention to when $Re_\lambda = 240$. At the outset, we notice from figure 4(b) that there is a rather very small set of scales that lies between the forcing scale ($k = 1$) and the scale where fluid dissipation becomes important ($k = 10$). Naturally, it cannot be expected that the lifetime of fluctuations τ_k is reliably estimated by relating it to the nonlinear flux via $\Pi_f \sim u_k^2/\tau_k$, as this relation does not account for losses due to viscous dissipation. However, it still estimates the rate at which energy is transferred to smaller scales. Noting that Π_f still has a power-law behaviour of $\Pi_f \sim k^{-1.4}$ in $k \in [3, 12]$ and $\Pi_p \approx \text{constant}$ in this range as well, we can now estimate the various time scales at $Re_\lambda = 240$ as

$$\tau_k \sim (ku_k)^{-1} \sim k^{-0.3}; \quad \tau_k \sim \frac{kE_k}{\Pi_f} \sim k^{0.1}; \quad \tau_k \sim \frac{kE_k}{\Pi_p} \sim k^{-1.3}. \quad (3.14)$$

We plot the corresponding compensated curves of these transfer time scales in [figure 5\(b\)](#). Consistent with our expectations, all of these curves are fairly constant in the rather small desired range $k \in [4, 10]$.

In a nutshell, the effect of the addition of polymers is to slow down the cascade process which we quantify using scaling arguments the knowledge of flux contributions, and the fluid energy spectra. In the next section, we discuss how energy is distributed in the polymeric scales of motion via the polymer energy spectrum using data as well as scaling arguments.

3.4. The polymer spectra

The distribution of energy across polymeric scales, in a statistically stationary state, can be obtained by computing the polymer energy spectrum $E_p(k)$ in analogy with the fluid energy spectrum $E(k)$. To do so, we start by defining the polymer energy spectrum in a sense similar to that of Casciola & De Angelis (2007), Balci *et al.* (2011) and Nguyen *et al.* (2016). The measure of average total polymer energy $\mathcal{E}_p$ is given by the $Tr(C)$ as

$$\mathcal{E}_p = \frac{\mu_p}{2\tau_p} \langle Tr(C) \rangle = \frac{\mu_p}{2\tau_p V} \int_V C_{ii}(\mathbf{x}) d\mathbf{x} = \frac{\mu_p}{2\tau_p V} \int_V B_{ij}(\mathbf{x}) B_{ji}(\mathbf{x}) d\mathbf{x}, \quad (3.15)$$

where B (with components B_{ij}) is the positive-definite square root of the conformation tensor C , i.e. $C_{ij}(\mathbf{x}, t) = B_{ik}(\mathbf{x}, t) B_{kj}(\mathbf{x}, t)$. One can now define the polymer energy spectrum $E_p(k)$ by employing Parseval's relation

$$\begin{aligned} \mathcal{E}_p &= \frac{\mu_p}{2\tau_p V} \int_V B_{ij}(\mathbf{x}) B_{ji}(\mathbf{x}) d\mathbf{x} = \frac{\mu_p}{2\tau_p V} \int_{\mathbb{R}^3} B_{ij}(\mathbf{k}) B_{ji}(-\mathbf{k}) d\mathbf{k} = \int_0^\infty E_p(k) dk \\ \text{where } E_p(k) &= \frac{\mu_p}{2\tau_p V} \int_{|\mathbf{k}|=k} B_{ij}(\mathbf{k}) B_{ji}(-\mathbf{k}) d\Omega_k, \end{aligned} \quad (3.16)$$

where V is volume of integration and the last integral is defined over a spherical shell of radius k .

Now, the scale-by-scale energy $(\mu_p/2\tau_p)C_k$ can then be estimated as the energy contained in the modes $\in [k, k + dk]$,

$$\frac{\mu_p}{2\tau_p} C_k = E_p(k) dk, \quad (3.17)$$

in analogy with the classical

$$\frac{1}{2} u_k^2 = E_k(k) dk. \quad (3.18)$$

Thus, it is easy to see using dimensional arguments that $C_k \sim k E_p(k)$, similar to $u_k^2 \sim k E_k(k)$. We now use this relation to estimate $E_p(k)$ by relating it with $E(k)$.

Let us begin by looking at the Π_p curves in [figure 3](#) (or [figure 4](#)). For large Re_λ , the flux contribution Π_p remains approximately constant for $k \in [20, 60]$. Therefore,

$$\frac{\mu_p}{\tau_p} k u_k C_k \sim k^0 \implies C_k \sim (k u_k)^{-1} \sim k^{-0.35}. \quad (3.19)$$

This immediately implies, using (3.17), that $E_p(k) \sim k^{-1} C_k \sim k^{-1.35}$ for $k \in [20, 60]$. Indeed, we find this to be consistent with the data from simulations plotted in [figure 6\(a\)](#). At $Re_\lambda \approx 240$, this scaling range of $E_p(k)$ shows a slight shift to larger scales, in correspondence to a similar shift of constant Π_p in [figure 4](#). We point out here that in contrast to the behaviour of $E(k)$, the scaling range for $E_p(k)$ appear cleaner with

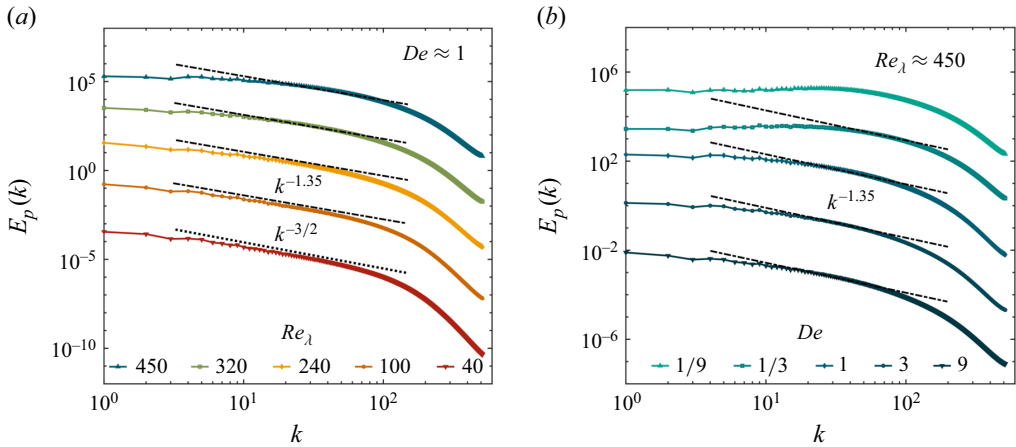


Figure 6. The dependence of the polymer energy spectrum $E_p(k)$ on (a) Re_λ (shown for $De \approx 1$), and on (b) De (shown for $Re_\lambda \approx 450$). The two different scaling regimes with exponents -1.35 (at large Re) and -1.5 (at small Re) are shown in dash-dotted and dotted lines, respectively. (b) Small De flows at large Re show a close to Newtonian behaviour and $E_p(k)$ remains devoid of any scaling form. As $De \gtrsim 1$, the expected scaling with exponent -1.35 begins to appear. The spectra are shifted vertically for visual clarity by factors of powers of 10.

decreasing Re_λ . This is because the assumption of $\Pi_p \sim k^0$ is not exactly true, especially for the largest Re_λ , and only provides a rough estimate of the self-similarity of $E_p(k)$. However, the scaling ranges get better with decreasing Re_λ also because the fluid nonlinearity becomes weaker and elastic effects begin to dominate the flux contributions. This is clearly brought out comparing figures 4(a) and 4(b). More importantly, these estimates are obtained by relating the polymer statistics to that of the fluid velocity field, i.e. the knowledge of one is required to obtain the other. However, the relation between these statistics changes at the smallest $Re_\lambda = 40$ where the fluid nonlinearity remains dormant and falls-off exponentially as shown in figure 4(c).

At the smallest $Re_\lambda \approx 40$, dissipative effects become dominant so that polymeric contribution $\mathcal{P}$ to the total flux is of the same order as $\mathcal{D}_f$ for $k \gtrsim 10$ in figure 4(c). Hence, a simple comparison of the fluid dissipation and polymer terms gives (see also Singh *et al.* 2024)

$$k^2 u_k \sim k C_k \implies E_p(k) \sim u_k \sim \sqrt{k E_k} \sim k^{-3/2}, \quad (3.20)$$

which is also consistent with the data shown in figure 6(a).

We now show the variation of the polymer spectrum with De in figure 6(b) for large Re_λ . At very small De , the polymers barely stretch and they quickly relax back to their equilibrium lengths. This means fluctuations in their lengths are largely limited to only small scales and minimal large-scale fluctuations. Thus, at relatively large scales and small k , for small De polymers, one expects a minimal growth in the spectrum of fluctuations making it appear rather flat. This can otherwise also be understood in terms of real space fluctuations as follows. In real space, as the polymers remain small, their fluctuations are localised to small scales as well such that their fluctuations are correlated over only small scales. So, at large separations, these fluctuations are decorrelated and appear as white noise. This gives the spectrum its flat shape over a wide range of k . However, at very large k , the spectrum $E_p(k)$ falls off much rapidly which is just a consequence of the small scales being well resolved and the polymer fields being analytic.

Now, as De increases, polymers begin to stretch to longer lengths, so that their fluctuations are now correlated over longer lengths whose effect begins to be seen in the spectrum being more pronounced at small k . At largest De , in a close agreement with the scaling arguments (3.19), we find that the spectrum $E_p(k) \sim k^{-1.35}$ for a wide range. The small scale fall-off of the spectra still confirms the analyticity of the polymer stress field.

We now move on to real space statistics, by first discussing the non-unique scaling nature using structure functions, complementing the discussion in § 3.1.

3.5. Velocity differences and structure functions

In this section, we discuss how a non-unique scaling behaviour is also manifested in the real-space statistics of PHIT. This complements the Fourier space discussion of § 3.1. One of the most common real-space measures that admit a scaling behaviour in turbulence are the well-known structure functions $S_p(r)$, defined as the p th moments of the longitudinal velocity increments $\delta_r u$ over a separation $\mathbf{r}$,

$$\delta_r u \equiv [\mathbf{u}(\mathbf{x} + \mathbf{r}) - \mathbf{u}(\mathbf{x})] \cdot \hat{\mathbf{r}}, \quad (3.21)$$

$$S_p(r) = \langle (\delta_r u)^p \rangle = \frac{1}{3} \sum_{i=1}^3 \langle [u_i(x_i + r_i) - u_i(x_i)]^p \rangle. \quad (3.22)$$

In particular, $S_2(r)$ is related to the energy spectrum $E(k)$ via a Fourier transform. For ease of arguments, we illustrate this using the vector second-order structure functions defined as (see (6.29), (6.40a) in Davidson (2015))

$$\langle [\mathbf{u}(\mathbf{x} + \mathbf{r}) - \mathbf{u}(\mathbf{x})]^2 \rangle \equiv \langle [\Delta \mathbf{u}]^2 \rangle = \frac{1}{r^2} \frac{\partial}{\partial r} [r^3 S_2(r)]. \quad (3.23)$$

The term on the left-hand side can be expanded as

$$\begin{aligned} \langle [\mathbf{u}(\mathbf{x} + \mathbf{r}) - \mathbf{u}(\mathbf{x})]^2 \rangle &= 2\langle u^2 \rangle - 2\langle \mathbf{u}(\mathbf{x} + \mathbf{r}) \cdot \mathbf{u}(\mathbf{x}) \rangle \\ &= 4 \int d\mathbf{k} |\hat{u}(\mathbf{k})|^2 - 4 \int d\mathbf{k} |\hat{u}(\mathbf{k})|^2 e^{-i\mathbf{k} \cdot \mathbf{r}} \\ &= 4 \int d\mathbf{k} E(k) \left(1 - \frac{\sin kr}{kr} \right) \end{aligned} \quad (3.24)$$

where we have the definition of Fourier transforms to obtain the second line and isotropy to obtain the last line. The previous relation can then be easily used to relate the power-law behaviour of S_2 and $E(k)$. Consider that the separation r in the real-space is scaled by a factor b , i.e. $r \rightarrow br$, so that the Fourier space wavenumber scales as $k \rightarrow b^{-1}k$. Consequently, if the spectrum scales with an exponent α , i.e. $E(k) \sim k^{-\alpha}$, then $E(k) \rightarrow E(b^{-1}k) = b^\alpha E(k)$. Therefore, the right-hand side of (3.24) can be rewritten under this rescaling as

$$\begin{aligned} \langle [\Delta \mathbf{u}]^2 \rangle_{rescaled} &= 4 \int (b^{-1} d\mathbf{k}) E(b^{-1}k) \left(1 - \frac{\sin kr}{kr} \right) \\ &= 4b^{\alpha-1} \int d\mathbf{k} E(k) \left(1 - \frac{\sin kr}{kr} \right) = b^{\alpha-1} \langle [\Delta \mathbf{u}]^2 \rangle. \end{aligned} \quad (3.25)$$

Thus, it is easy to see that the vector and longitudinal structure functions transform identically under rescaling since

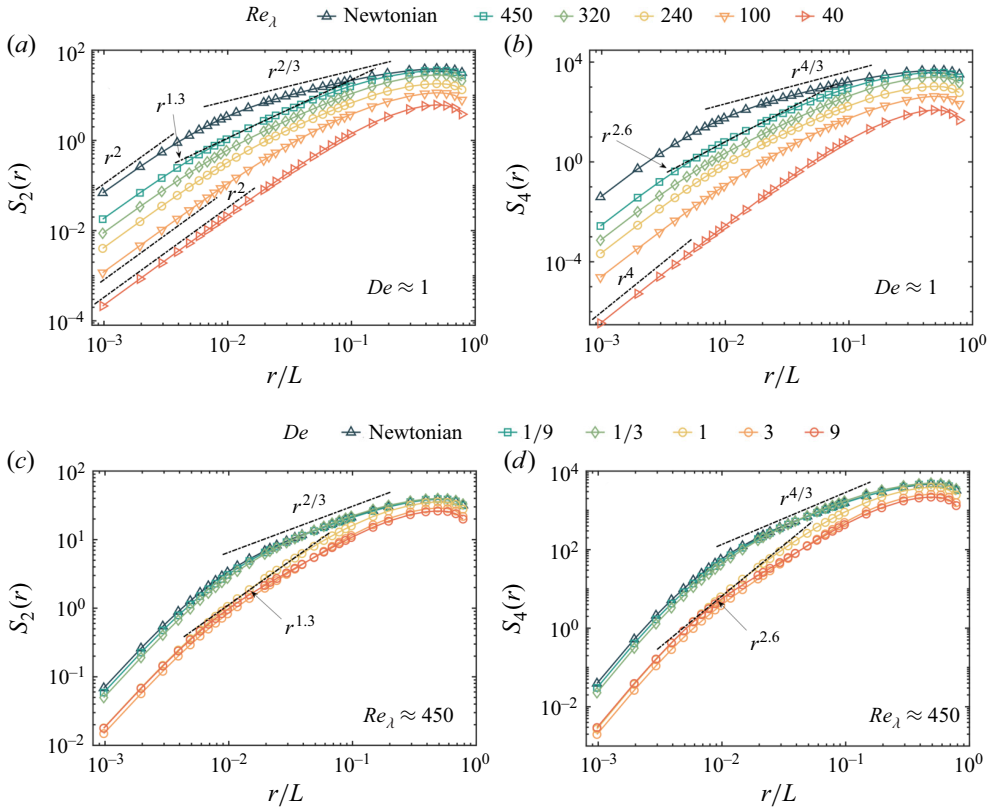


Figure 7. Manifestation of the non-unique scaling behaviour in the structure functions of second (S_2 ; panels (a) and (c)) and fourth (S_4 ; panels (b) and (d)) orders. Panels (a) and (b) show the dependence on Re_λ , while panels (c) and (d) show the dependence on the polymer elasticity De . Note that the (c) $S_2(r)$ and (d) $S_4(r)$ curves fall on top of the Newtonian for small De . At large De , the elastic scaling regime becomes clear as elasticity begins to play a significant role showing a clear departure from the Newtonian curve.

$$\begin{aligned} \langle [\Delta \mathbf{u}]^2 \rangle_{rescaled} &= \frac{1}{(br)^2} \frac{\partial}{\partial (br)} [(br)^3 S_2(br)] = \frac{1}{r^2} \frac{\partial}{\partial r} [r^3 S_2(br)] \\ &= b^{\alpha-1} \langle [\Delta \mathbf{u}]^2 \rangle = \frac{1}{r^2} \frac{\partial}{\partial r} [r^3 b^{\alpha-1} S_2(r)] \implies S_2(br) = b^{\alpha-1} S_2(r). \end{aligned} \quad (3.26)$$

Hence, we have that $E(k) \sim k^{-\alpha} \iff S_2(r) \sim r^{\alpha-1}$. Note that this relation holds only for $\alpha \leq 3$. For $\alpha > 3$, the real-space exponent is constrained by the leading order in Taylor expansion as $S_2 \sim r^2$. In HIT, these arguments imply that $S_2 \sim r^{2/3}$ given $E(k) \sim k^{-5/3}$ whereas in PHIT we now expect $S_2 \sim r^{1.3}$ using $E(k) \sim k^{-2.3}$. Additionally, using dimensional arguments, one also expects within the K41 phenomenology that $S_4 \sim S_2^2$. With these expected results in mind, we show in figure 7(a,b) the plots of $S_2(r)$, $S_4(r)$ for PHIT at different Re_λ and $De \approx 1$ alongside the HIT result. The variation of $S_2(r)$ and $S_4(r)$ with De is shown in figure 7(c,d). We of course have that the HIT structure functions follow the Kolmogorov scaling $r^{p/3}$ closely in figure 7(a,b), while those for PHIT show a very clear departure from this behaviour. Indeed, and in consistency with the discussion above, the polymeric scaling is given by $S_2 \sim r^{1.3}$ ($S_4 \sim r^{2.6}$) and is seen to have the widest span at the largest $Re_\lambda \approx 450$. This is also consistent with the discussion in § 3.1 where we show that the polymeric regime shrinks with decreasing Re_λ , while

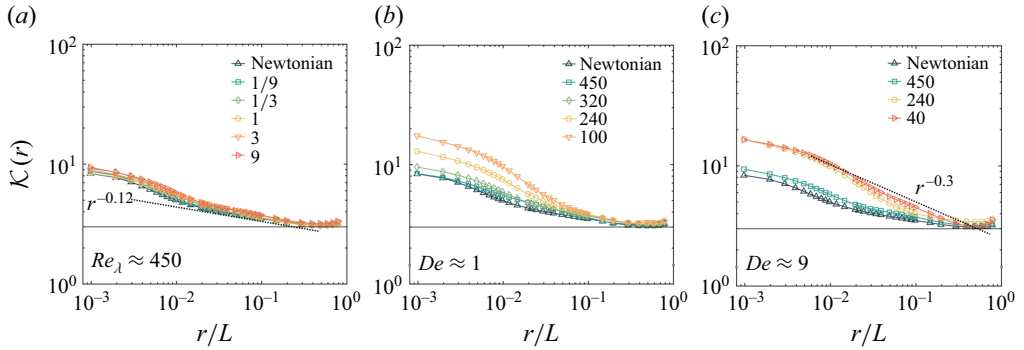


Figure 8. The kurtosis of velocity differences as a function of scale r . Here $\mathcal{K} \rightarrow 3$ as $r \rightarrow L$ as velocity differences decorrelate at very large separations. (a) Here $\mathcal{K}$ at large $Re_\lambda \approx 450$ and different De are almost coincident implying a very weak dependence of intermittency on De . (b,c) Intermittency in polymeric flows increases as Re_λ is decreased, especially when De is large.

the smooth dissipation range marked by $S_2 \sim r^2$ expands (corresponding to $E(k) \sim k^{-4}$ in figure 2). At the smallest $Re_\lambda \approx 40$, the smooth scaling $S_2 \sim r^2$ spans almost a decade.

We show the variation of the structure functions with De in figure 7(c,d). As expected from figure 2(a), this dependence is rather non-monotonic. The small De cases show an approximately Newtonian behaviour, owing to the minimal non-Newtonian contributions as the polymers strongly resist any stretching (see § 3.1 for detailed discussion). As $De \rightarrow 1$, we have a clear polymeric scaling $S_2 \sim r^{1.3}$ ($S_4 \sim r^{2.6}$). This steeper than Kolmogorov slope starts to vanish when polymer elasticity is further increased, and the S_2/S_4 curves now have a shallower slope. At much larger polymer elasticity one indeed recovers the Kolmogorov scaling (see Rosti *et al.* (2023)). This behaviour is again in consistency with that for the spectrum in § 3.1.

We also make an important note about figure 7(b,d). The $S_4(r)$ curves evidently show smaller scaling ranges compared with those of $S_2(r)$ in figure 7(a,c). This means that the exponents quickly deviate from the naïve expectation of $S_4(r) \sim S_2^2(r)$. This is not only an artefact of the deviations from a K4-like behaviour but also captures the non-Gaussianity of $\delta_r u$. We quantify these deviations by measuring the kurtosis of the velocity increment distributions in the next section.

3.6. Kurtosis of velocity differences

Consider the distribution of (longitudinal) velocity differences $\delta_r u$, defined by (3.21), as a function of the scale r . The kurtosis (or flatness) $\mathcal{K}(r)$ of such a distribution is defined as

$$\mathcal{K}(r) \equiv \frac{\langle (\delta_r u)^4 \rangle}{\langle (\delta_r u)^2 \rangle^2}. \quad (3.27)$$

The kurtosis $\mathcal{K}$ captures the relative importance of the tails of a distribution and quantifies their contribution to the overall statistics of $\delta_r u$. For a Gaussian distribution, $\mathcal{K} = 3$. We expect the velocity increments to be uncorrelated over very large separations, so that the distribution of $\delta_r u$ is close to a Gaussian for large r . This is indeed confirmed in our data in figure 8 where we find $\mathcal{K}(r) \approx 3$ for large r , irrespective of Re_λ and De . More importantly, $\mathcal{K}$ is not a constant but a function of the scale r . The distributions of $\delta_r u$ are, evidently, devoid of scale-invariance and their departures from Gaussianity become increasingly stronger at small r . This is a result of more important contributions from the tails of the distribution of $\delta_r u$, a phenomenon referred to as intermittency, and causes

deviations from the dimensional expectation of $S_4 \sim S_2^2$ (this would have meant $\mathcal{K} \sim r^0$ from (3.27)). The log–log plots of $\mathcal{K}$ in figure 8(a) clearly show a power-law dependence on r at large $Re_\lambda \approx 450$. Crucially, this power-law is very weakly dependent on De as the curves for different De follow each other closely. Thus, the intermittent nature of the velocity fluctuations is still largely determined by the fluid nonlinearity. This was also observed by Rosti *et al.* (2023) via the multifractal spectrum for energy dissipation. The influence of polymers on velocity fluctuations, however, is more apparent at small Re_λ , as shown in figure 8(b). At small Re_λ , although the fluid nonlinearity becomes considerably weaker (see figure 4b), the polymer stresses feeding back on the flow result in the velocity fluctuations $\delta_r u$ being more intermittent, and the departure from HIT curve becomes significant. This is even more pronounced at the smallest Re_λ (we considered) where the presence of polymers results in much large deviations of $\delta_r u$ at small r which is manifested in a much steeper slope of the kurtosis $\mathcal{K}(r) \sim r^{-0.3}$ compared with the Newtonian.

So, the departure from a Kolmogorov-like behaviour in polymeric flows is not only due to a modified energy flux – resulting in a different scaling of the spectrum – but also due to the modified nature of extreme fluctuations that result from the action of the polymer stresses. This also underlines the fact that intermittency is due not only to fluid nonlinearity but even polymer stresses can drive highly intermittent velocity fluctuations. Such intermittent behaviour is also discernible in the statistics of velocity gradients. In the following sections, we discuss the intermittent nature of velocity gradients, and how they influence the stretching of polymers. This also forms the basis for the discussion of the two energy dissipation rates: fluid ϵ_f and polymer ϵ_p .

3.7. Polymer stretching, velocity gradients and their relation to the energy dissipation

We now discuss in this section how polymers of different De are themselves affected by the fluid flow at different Re_λ . To this end, we begin by simply looking at the stretching statistics of the polymers, the measure of the stretching of the polymers is their end-to-end lengths whose instantaneous squared value is given by $Tr(\mathbf{C})$. We naturally expect polymers to stretch more with increasing De at any given Re_λ . As stated earlier, in the limit of $De \rightarrow 0$ the polymers are almost inextensible and $\mathbf{C}$ does not stray far away from its equilibrium configuration $\mathbf{I}$. On the contrary, the other limit of $De \rightarrow \infty$ implies a weak restoring force, allowing $\mathbf{C}$ to grow to large values. That is, polymers take a very long time to relax back to their equilibrium lengths for a very large τ_p . Or in other words their tendency to relax back, when extended, is much less. Evidently, polymers are stretched by the local velocity gradients given by the first two terms on the right-hand side of (2.1b).

We plot the p.d.f.s of $Tr(\mathbf{C})$ for different Re_λ in figure 9. We first note that although polymers described by the Oldroyd-B model are infinitely stretchable, they can only do so in the presence of very large and sustained velocity gradients. This is confirmed by the very fast decay of the tails of the $Tr(\mathbf{C})$ -p.d.f.s in figure 9, clearly suggesting that the polymer lengths always remain bounded in our simulations. Figure 9(a) shows that, at large Re_λ , the p.d.f.s shift towards the right with increasing De indicating a larger averaged polymer length. Moreover, the width of the distributions also increases with De , meaning that polymer lengths also fluctuate over a wider range. This is more accurately shown by figure 10 where we plot the mean ($\mu_{Tr(\mathbf{C})}$) and standard deviation ($\sigma_{Tr(\mathbf{C})}$) of the distributions as a function of Re_λ and De . Indeed, the polymer lengths and their fluctuations increase with both Re_λ and De .

Figures 9(b) and 9(c) show the $Tr(\mathbf{C})$ distributions for smaller Re_λ . With decreasing Re_λ , turbulence intensity decreases and the velocity gradients become weaker on an average and stretch the polymers less (as can be seen from (2.1b)). Therefore, the mean

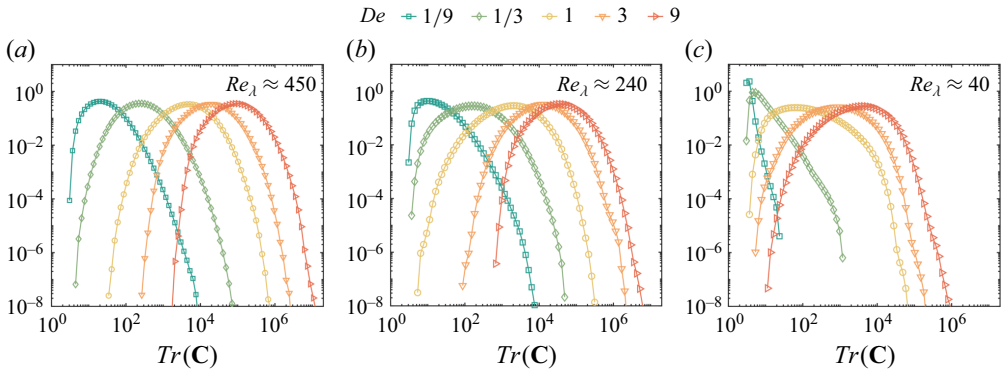


Figure 9. Probability distribution functions (p.d.f.s) of the end-to-end polymer lengths $Tr(C)$ for different Re_λ : (a) $Re_\lambda \approx 450$, (b) $Re_\lambda \approx 240$ and (c) $Re_\lambda \approx 40$ and all De . A large De polymer has a larger average end-to-end length, as seen in the right shift of the p.d.f.s.

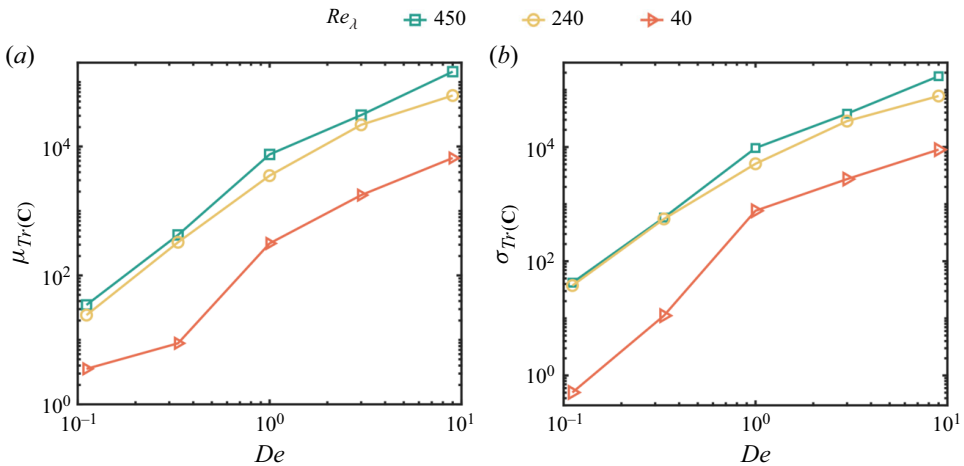


Figure 10. (a) Mean $\mu_{Tr(C)}$ and (b) standard deviation $\sigma_{Tr(C)}$ of the distributions in figure 9, shown as a function of Re_λ and De .

polymer lengths decrease with decreasing Re_λ as the p.d.f.s shift towards smaller values of $Tr(C)$. Moreover, polymers are also limited in their maximum extensions as Re_λ decreases. At the smallest Re_λ , the velocity gradients are unable to stretch the less extensible, small De polymers considerably. This is captured in figure 9(c), where the $Tr(C)$ -p.d.f.s fall-off very fast at small De showing that polymer lengths have rather small fluctuations. (This also implies that polymer stresses remain very small so that the flow remains laminar for $De < 1$). However, for a large enough De (≈ 1), polymers stretch to considerably long lengths, and the resulting large fluctuations are enough to excite subdominant velocity fluctuations which gives rise to ET with $E(k) \sim k^{-4}$ (see figure 2).

The above discussion is largely based on how polymers with different De are stretched by carrier flows at different Re_λ . To understand this better, we now discuss how the polymer stretching $Tr(C)$ is correlated with the velocity gradients $A_{ij}(\mathbf{x}, t) \equiv \partial_i u_j(\mathbf{x}, t)$ in the flow. To this end, we first decompose A_{ij} into its symmetric S_{ij} and antisymmetric ω_{ij} components that, respectively, capture the purely extensional (compressional) and the

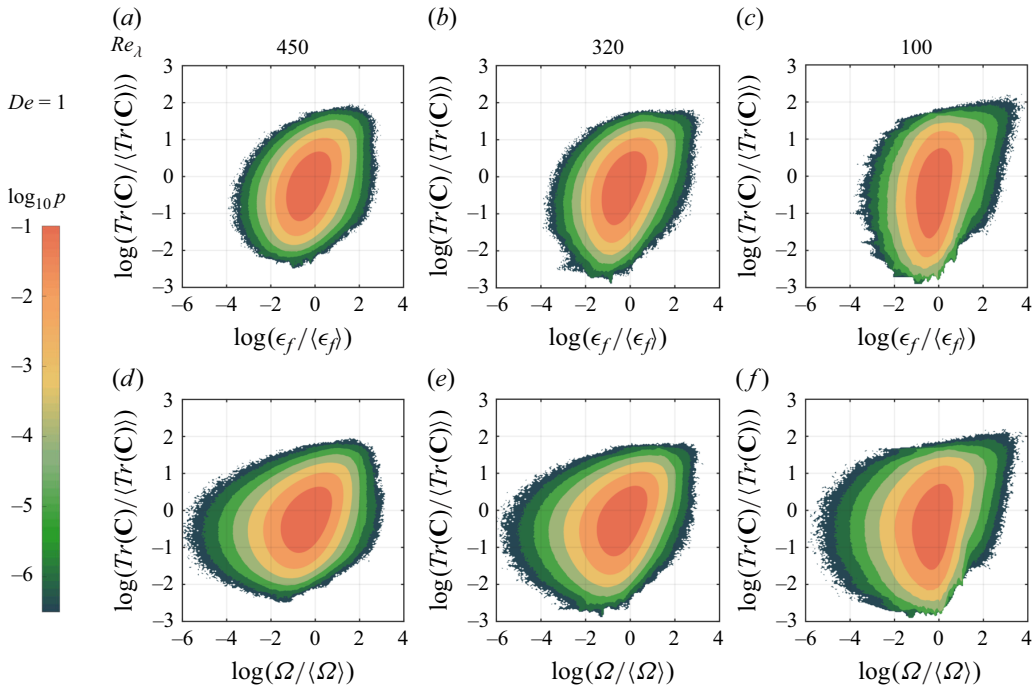


Figure 11. The plot of the joint distributions of the polymer lengths on log–log scale with the (a–c) dissipation rate ϵ_f and (d–f) entropy Ω , for different Re_λ with $De \approx 1$. The colour bar shows the colour coding of the logarithm of probability $\log_{10} p$.

purely rotational contributions. The squared magnitude of these components are given by the fluid dissipation rate ϵ_f and enstrophy Ω ,

$$\begin{aligned} \Omega &= \omega_{ij}\omega_{ij}; & \epsilon_f &= 2\nu S_{ij}S_{ij}, \\ \text{where } \omega_{ij} &= (\partial_i u_j - \partial_j u_i)/2; & S_{ij} &= (\partial_i u_j + \partial_j u_i)/2. \end{aligned} \quad (3.28)$$

The presence of the symmetric term $\mathbf{C}\nabla\mathbf{u} + (\nabla\mathbf{u})^T\mathbf{C} = 2C_{ik}S_{kj}$ in (2.1b) means that the extensional (compressional) regions of the flow are directly responsible for the stretching (relaxation) of the polymers. On the other hand, the absence of any ω_{ij} terms means that there is no direct effect of the rotation in changing the lengths of polymers. However, turbulence in three dimensions is marked by the stretching and intensification of vorticity in the direction of local velocity gradients. So, the vortical regions can be expected to correlate with large polymer lengths, although to a lesser degree than the straining regions. (A direct computation of Pearson correlation coefficients of the joint distributions of $(\text{Tr}(\mathbf{C}), \epsilon_f)$ as well as those of $(\text{Tr}(\mathbf{C}), \Omega)$ yielded values ≈ 0.3 for all cases, while those of the log of normalised variables which are actually studied, e.g. of $(\log[\text{Tr}(\mathbf{C})/\langle \text{Tr}(\mathbf{C}) \rangle], \log[\epsilon_f/\langle \epsilon_f \rangle])$, yielded values ≈ 0.4 showing that indeed these variables have a non-zero, finite correlation.)

To illustrate the above, we show in figure 11 the joint p.d.f.s (j.p.d.f.s) of the polymer lengths (given by $\text{Tr}(\mathbf{C})$) with the local stretching rates (given by ϵ_f) as a function of Re_λ for one instance of polymer elasticity of $De = 1$ in figure 11(a–c). We observe that the longest end-to-end lengths of the polymers indeed coincide with the largest stretching rates, while the smallest polymers are found in regions of the flow with small extensional rates. This results in a perceivable tilt of the joint distribution in figure 11(a). With decreasing Re_λ , the mean lengths of the polymers decreases (see figure 10) and

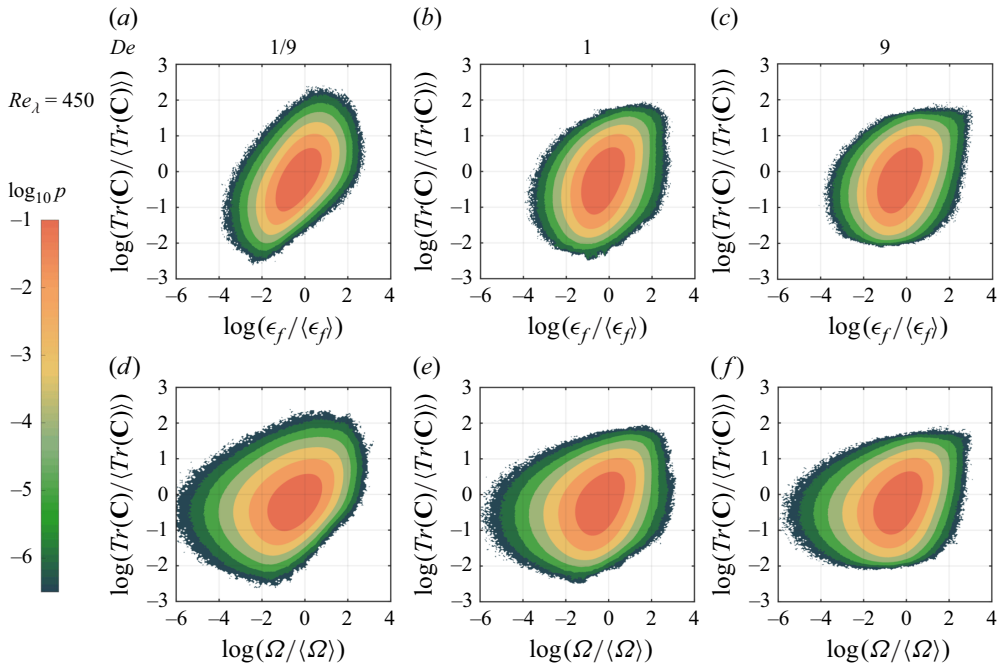


Figure 12. Joint distributions of the polymer lengths with the (a–c) ϵ_f and (d–f) Ω , for different De at $Re_\lambda \approx 450$. Different colours correspond to the logarithm of probability $\log_{10} p$ as coded by the colourbar.

their preference for regions with small-scale fluctuations increases. This is evident from figure 11(b,c) where elongated bottom tails of the j.p.d.f.s imply small polymer lengths are more probable at smaller Re_λ . While we still have that the largest polymer extensions coincide with the largest velocity gradients, the core of the j.p.d.f.s is now more vertical which indicates that much larger extensions are now possible at even the average stretching rates. This hints towards a decreasing degree of correlation between extreme stretching rates and polymer stretching as Re_λ is reduced.

Figure 11(d–f) show the j.p.d.f.s of $Tr(C)$ and enstrophy Ω . At large Re_λ , large polymer lengths also coincide with extreme vorticity regions. This means polymers are also stretched in regions of large vorticity (similar to what observed for long, polymer-like fibres in Picardo *et al.* (2020)). The maximum enstrophy regions, however, are more likely to have polymers with close to average lengths, implied by figure 11(d), unlike the straining regions whose extremes see maximally extended polymers. More importantly, polymers are likely to be stretched even in regions with very small Ω as suggested by the left bulge of the j.p.d.f.s. This shows that the polymer stretching–enstrophy correlation is not as strong as the stretching–straining correlation. This is even more evident with decreasing Re_λ as vortex stretching becomes progressively weaker. Indeed, figure 11(f) shows that polymer lengths are rather uniformly distributed, especially for small enstrophy, indicating an even less correlation with polymer stretching.

Figure 12 shows instead how polymer stretching correlates with the local stretching rates (figure 12a–c) and rotation rates (figure 12d–f) of the flow, as a function of polymer elasticity. It was already shown that large De polymers stretch more and is clearly captured by their mean lengths in figure 10. At small De , polymers stretch minimally and have small relaxation times. Therefore, while they are stretched by regions with very large stretching rates, those regions have rather small lifetimes (a quick estimate gives $\tau \sim S_{ij}^{-1}$).

So, maximally stretched polymers are more likely to persist for longer in regions with moderate stretching rates. This means that the maximum of $Tr(\mathbf{C})$ coincides with only slightly larger than the average values of $\langle \epsilon_f \rangle$. However, at larger De , polymers are more stretchable and easily acquire their maximal lengths upon encountering strong straining regions (similar to the observation in Singh (2024) that long, elastic, polymer-like fibres preferentially sample straining regions). At these large De , polymers remain stretched for longer times so that the fluctuations about the mean become smaller, across all values of ϵ_f , thus giving the j.p.d.f.s more rounded contours. Figure 12(d–f) plots the $Tr(\mathbf{C}) - \Omega$ joint distributions. We, of course, again have a much wider spread of the distributions compared with $Tr(\mathbf{C}) - \epsilon_f$, yet again suggesting that enstrophy and polymer stretching are less correlated compared with $\epsilon_f - Tr(\mathbf{C})$, as polymers can also be stretched when enstrophy is very small. Thus, while the maximally stretched polymers are most likely found in regions with maximal enstrophy at large De , they also tend to be stretched in regions with very small Ω when De is large.

3.8. Energy dissipation

In this last section, we discuss how the nature of energy dissipation in turbulence is modified in the presence of polymers. In polymeric flows, energy is dissipated away by both the carrier fluid ϵ_f and the dissolved polymers ϵ_p . The positive-definite fluid dissipation is given by $\epsilon_f = 2\nu S_{ij}S_{ij}$, whereas the positive-definite polymeric dissipation is related to the average end-to-end polymer length by $\epsilon_p = (\mu_p/2\tau_p^2) \langle Tr(\mathbf{C}) - 3 \rangle$. Both these relations can be readily obtained by multiplying (2.1a) with $\mathbf{u}$, and using (2.1b) as follows:

$$\begin{aligned} \partial_t \langle \mathbf{u}^2 \rangle / 2 &= \nu \langle \mathbf{u} \nabla^2 \mathbf{u} \rangle + \frac{\mu_p}{\tau_p} \langle \mathbf{u} \cdot \nabla \cdot \mathbf{C} \rangle = -\nu \langle (\nabla \mathbf{u})^2 \rangle - \frac{\mu_p}{\tau_p} \langle Tr[\mathbf{C} \nabla \mathbf{u}] \rangle + \langle \mathbf{F} \cdot \mathbf{u} \rangle \\ \implies 0 &= -2\nu \langle S_{ij}S_{ij} \rangle - \frac{\mu_p}{\tau_p} \langle Tr[\mathbf{C} \nabla \mathbf{u}] \rangle + \langle \mathbf{F} \cdot \mathbf{u} \rangle = -\epsilon_f - \epsilon_p + \epsilon_I. \end{aligned} \quad (3.29)$$

Similarly,

$$\begin{aligned} \mu_p \partial_t \langle \mathbf{C} \rangle &= \mu_p \langle \mathbf{C} (\nabla \mathbf{u}) \rangle + \mu_p \langle (\nabla \mathbf{u})^T \mathbf{C} \rangle - \frac{\mu_p}{\tau_p} \langle \mathbf{C} - \mathbf{I} \rangle \\ \implies 0 &= \frac{2\mu_p}{\tau_p} \langle Tr[\mathbf{C} \nabla \mathbf{u}] \rangle - \frac{\mu_p}{\tau_p} \langle Tr(\mathbf{C}) - 3 \rangle \implies \epsilon_p = \frac{\mu_p}{2\tau_p^2} \langle Tr(\mathbf{C}) - 3 \rangle, \end{aligned} \quad (3.30)$$

where we have used stationarity, periodicity and incompressibility to set time derivatives, fluid nonlinearity, pressure contribution and polymer advection terms to zero. Note that, the previous relation $\epsilon_p = (\mu_p/\tau_p) \langle Tr[\mathbf{C} \nabla \mathbf{u}] \rangle = (\mu_p/2\tau_p^2) \langle Tr(\mathbf{C}) - 3 \rangle$ holds true only on average, and thus the two processes are equal only in a statistically stationary state, but very different instantaneously. The $Tr[\mathbf{C} \nabla \mathbf{u}]$ term captures the exchange of energy between fluid and the polymers, and can take both positive and negative values, while $\langle Tr(\mathbf{C}) - 3 \rangle$ is a positive-definite quantity and captures purely dissipative effects. The interaction term $(\mu_p/\tau_p) Tr[\mathbf{C} \nabla \mathbf{u}]$ leads to a net transfer of energy to polymers, which is dissipated away as $(\mu_p/2\tau_p^2) \langle Tr(\mathbf{C}) - 3 \rangle$. This is seen from figure 13, where we plot the normalised distributions of the two terms using data from our simulations. The positive-definiteness of ϵ_f and ϵ_p means that the total energy injected by the forcing ϵ_I is dissipated away by both polymers and the fluid in a stationary state. The internal energy of the polymers is proportional to their instantaneous extension so that elongated polymers dissipate away energy as they relax. We now discuss the nature of these measures of dissipation in our polymeric flows.

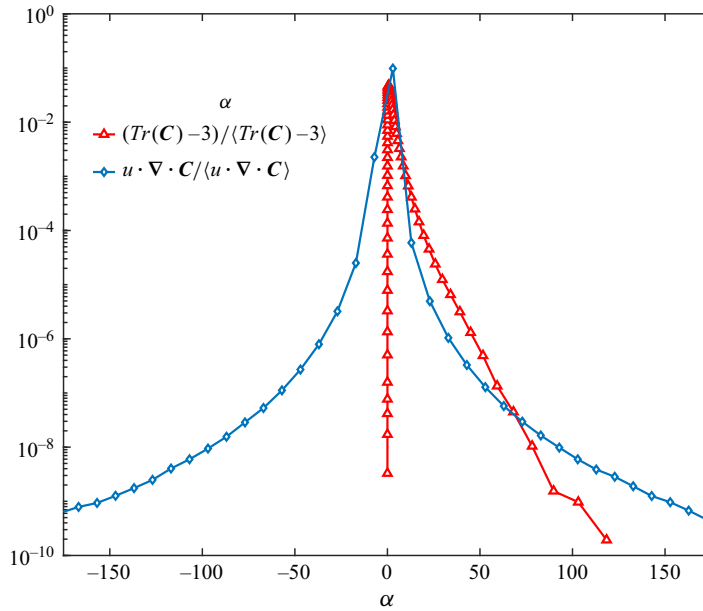


Figure 13. The p.d.f.s comparing the local dissipation and transfer processes associated with polymers. They equal each other only on an average, while locally the processes are very different.

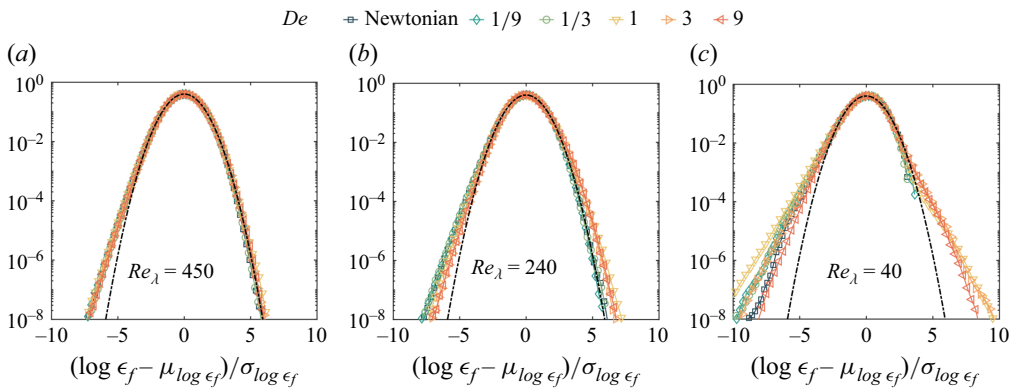


Figure 14. The p.d.f. of the fluid energy dissipation rate ϵ_f , compared with a log-normal distribution, for different De and Re_λ . At (a) $Re_\lambda \approx 450$, polymer elasticity has no influence on the intermittent nature of the distributions. However, at smaller (b) $Re_\lambda \approx 240$, the presence of large De polymers leads to more large deviations, which are even more prominent at (c) $Re_\lambda \approx 40$.

We first recall that ϵ_f in HIT has a distribution whose tails deviate from a log-normal behaviour, in contradiction to the Kolmogorov (1962) prediction. We now show in figure 14(a) that the normalised $\log(\epsilon_f)$ -p.d.f.s remain largely unaffected by the addition of polymers in flows at large Re_λ . The curves for different De all collapse over the Newtonian curve in figure 14(a) which shows that spatiotemporal fluctuations in energy dissipation are unaffected by the addition of polymers. Polymer stresses, though present, do not result in yet larger deviations which are still dominated by the fluid nonlinearity. (Note that the mean fluid dissipation $\langle \log \epsilon_f \rangle$ is still a function of De .) At a smaller $Re_\lambda \approx 240$, the Newtonian curve shows an even larger deviation from log-normality,

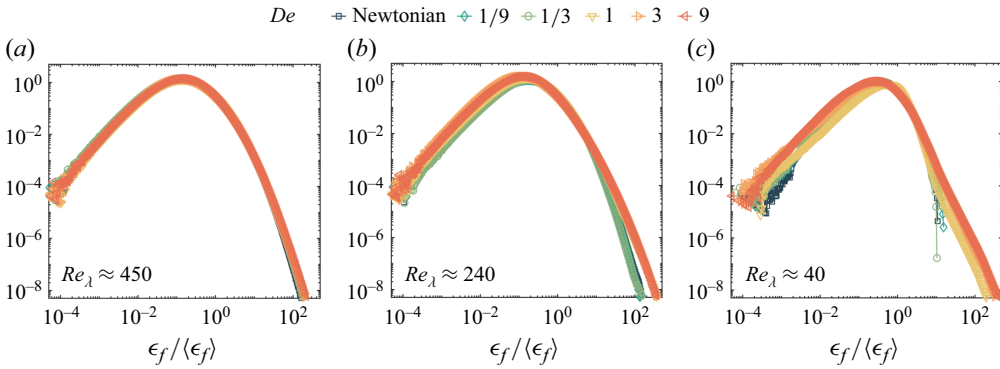


Figure 15. The p.d.f. of the fluid energy dissipation rate ϵ_f for different De and Re_λ . Each panel corresponds to a decreasing Re_λ from (a) to (c), for all the investigated De .

especially at the left tails, suggesting that dissipation field now has relatively more quiescent regions. There is no appreciable change in the distributions upon the addition of small De polymers as the polymer stresses remain small. However, when De is large, elastic effects become appreciable compared with the weakened fluid nonlinearity. The polymer stresses are now large enough to create significant fluctuations in the flow so that now there are less quiescent regions and more extreme events. This is apparent from the shrinking left tails and the widening right tails at $De = 1, 3$ in figure 14(b). Curiously, at the largest $De = 9$, when the elastic effects begin to weaken again, the large deviations are reduced (this is in parallel to the weakened elastic effects resulting in the shrinking polymeric range in figure 2b). These effects are most clearly seen at the smallest $Re_\lambda = 40$ where fluid nonlinearity does not play a role (and decays exponentially in scales, see figure 4c). The fluctuations in velocity gradients, therefore, only result from the strong polymer stresses at large De and are manifested in the wide-tailed, super log-normal distributions of ϵ_p in figure 14(c). However, for a large polymer elasticity such as $De = 9$, a weakening of elastic effects results in a mild shrinking of the tails of the p.d.f. Figure 15 shows the normalised p.d.f.s of the bare ϵ_f for three different Re_λ and all De . It is clear from these plots that at large Re the presence of polymers does not affect the nature of extreme events in polymer dissipation, which overlap to the Newtonian curve. This is to say the intermittency corrections are the same in Newtonian and polymeric turbulence at large Re , consistently with the collapse of the multifractal spectra presented by (Rosti *et al.* 2023). The differences begin to surface at smaller Re where extreme events become more prominent, especially at large De . This is again consistent with the kurtosis picture in figures 8(b) and 8(c), where the curves steepen at large De and small Re . A crucial difference with figure 14 is seen at $Re_\lambda = 40$, where the log-normal plot shows that the dissipation distributions vary non-monotonically with De , whereas figure 15 shows that the dependence is monotonic.

We show the distributions of the polymer dissipation ϵ_p in figure 16, which are sublognormal, unlike ϵ_f , thus indicating a significantly less intermittent behaviour. In particular, at small De , ϵ_p shows more large deviations. These polymers rarely stretch and even when stretched, they quickly relax back to their small, equilibrium lengths. This means any deviations about a small mean are more significant. Thus, the polymer dissipation $\epsilon_p \propto Tr(C)$ shows the widest tails at the smallest $De = 1/9$, which are wider than even a log-normal distribution, especially at larger Re_λ in figure 16(a,b). With increasing De polymers tend to stretch more and for longer duration owing to the larger relaxation times. Thus, fluctuations in lengths become less important at large

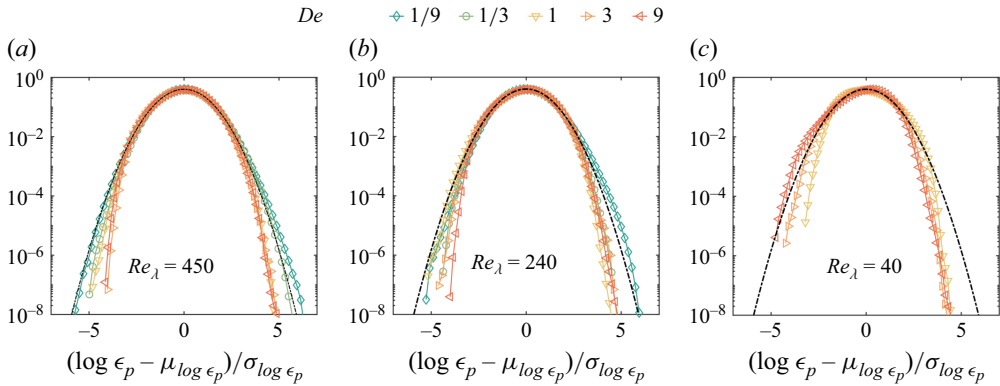


Figure 16. The p.d.f. of the logarithm of polymer dissipation $\epsilon_p \propto \text{Tr}(\mathbf{C})$, as a function of De for different Re_λ given in the panels. The black dashed curve shows a log-normal distribution for reference. The polymer dissipation becomes less intermittent with increasing De .

De , and consequently, the stored energy is dissipated away in a more uniform and less intermittent manner, with fewer large deviations. This results in the $\log \epsilon_p$ distributions becoming progressively sublognormal. This effect is rather persistent across all Re_λ , even into the ET regime at $Re_\lambda \approx 40$, as seen from figure 16.

4. Conclusions

In this work, we investigate how various measures that typically characterise classical, Newtonian turbulence behave in polymeric flows as both elasticity and inertia of the flow are varied, especially focusing on how the large and small Re regimes connect at intermediate Reynolds numbers. While turbulence statistics indeed depend on both Re and De , which quantify fluid inertia and polymer elasticity, respectively, we show that the addition of polymers has contrasting effects on different turbulence statistics.

We begin by showing that the energy spectrum in polymeric flows shows a non-unique scaling nature, especially at large Re and moderate De , where three different dominant flux contributions – *viz.* fluid nonlinearity, polymeric and the dissipative contributions – lead to three distinct scaling exponents. This non-unique scaling behaviour is invariably lost at both very large and very small polymer elasticity, where instead the Newtonian behaviour is recovered similar to the observation by Rosti *et al.* (2023). With decreasing Re_λ , the Newtonian and polymeric regimes are progressively lost as the fluid inertia weakens and viscosity becomes more important. A unique, smooth, dissipative, ET regime spans a wide range of scales at very small Re_λ , when polymer elasticity is large. We further shed light on the dynamics of our polymeric flows by estimating the typical lifetimes of velocity fluctuations, and the rates of energy transfer to smaller fluid scales and to the polymeric mode. We use scaling arguments to show that the classical fluid energy cascade is slowed and weakened in the presence of polymers. The real space statistics of velocity fluctuations, captured by the structure functions, also admit different scaling exponents that are directly related to the Fourier space scaling of the energy spectra.

The real space statistics also additionally reveal the intermittent nature of velocity fluctuations in polymeric flows. At very large Re_λ , the presence of polymers has almost no effect on the kurtosis of fluctuations. However, with decreasing Re_λ , elastic stresses become increasingly more important than the fluid nonlinearity and result in strongly intermittent velocity fluctuations. The relative importance of polymer stresses is made

clear by the end-to-end polymer lengths that are given by the trace of the conformation tensor. As expected, polymers stretch more as their elasticity increases and they are able to span a wide range of scales. We further study how polymers stretch in different regions of the flow by decomposing velocity gradients into extensional and rotational components. Extensional regions, quantified by the symmetrised velocity gradients, promote the stretching of the polymers, whereas the local rotation rates, quantified by enstrophy, play a rather indirect role in their stretching. While we indeed find that local rotation rates correlate with large polymer lengths, since velocity gradients intensify vorticity by stretching them in their direction, polymers are shown to also stretch in regions with small rotation rates, thus indicating a lesser correlation between enstrophy and polymer lengths.

Finally, we relate polymer lengths and velocity gradients to the energy dissipated away by the carrier fluid and the polymers, and compare them with a log-normal distribution. At large Re_λ , much like the kurtosis of velocity fluctuation, fluctuations of fluid dissipation remain unchanged upon the addition of polymers. However, polymer stresses become important at small Re_λ and result in large deviations in fluid dissipation. The effect of polymers is most clear at the smallest Re_λ where the fluid nonlinearity is inactive and yet the fluid dissipation distribution is very far from log-normal. On the other hand, dissipation by polymers themselves is much less intermittent compared with the fluid dissipation, with tails shrinking even further as polymer elasticity increases. This is because polymers are able to stretch more uniformly and hence dissipate away their stored energy in a less intermittent, more uniform fashion. While this analysis relates the local strain and rotation rates to the stretching of polymers, it is known that the Lagrangian history of these quantities can also be crucial in determining the behaviour of polymer stresses, as shown in the works of Wagner & McKinley (2016), and Kumar, Guasto & Ardekani (2023). Future Lagrangian studies on PHIT should better shed light on how closely polymer stresses mirror the local flow topology across such a wide range of Re and De numbers.

With this work, we have connected polymeric turbulence at large Reynolds number with ET, where inertia effects are vanishing. While the two regimes show substantial differences, as for example clearly indicated by the non-unique scaling behaviour of the energy spectra, the transition between the two is rather smooth and continuous in the chosen framework of homogeneous and isotropic turbulence. Future work should deal with better characterising and explaining the origin of the various identified exponents of the energy spectra, as well as extending the analysis to more complex flows.

Funding. The research was supported by the Okinawa Institute of Science and Technology Graduate University (OIST) with subsidy funding to M.E.R. from the Cabinet Office, Government of Japan. M.E.R. also acknowledges funding from the Japan Society for the Promotion of Science (JSPS), grants 24K00810 and 24K17210. The authors acknowledge the computer time provided by the Scientific Computing and Data Analysis section of the Core Facilities at OIST, and the computational resources provided by the HPCI System (project IDs: hp250035, hp230018, hp220099, hp210269 and hp210229). R.K.S. thanks Alessandro Chiarini (OIST) for discussions and suggestions.

Declaration of interests. The authors report no conflict of interest.

REFERENCES

- ABDELGAWAD, M.S., CANNON, I. & ROSTI, M.E. 2023 Scaling and intermittency in turbulent flows of elastoviscoplastic fluids. *Nat. Phys.* **19**, 1059–1063.
- ASWATHY, M.S. & ROSTI, M.E. 2024 The dynamics of fibres dispersed in viscoelastic turbulent flows. *J. Fluid Mech.* **984**, A72.
- BAGHERI, F., MITRA, D., PERLEKAR, P. & BRANDT, L. 2012 Statistics of polymer extensions in turbulent channel flow. *Phys. Rev. E* **86**, 056314.
- BALCI, N., THOMASES, B., RENARDY, M. & DOERING, C.R. 2011 Symmetric factorization of the conformation tensor in viscoelastic fluid models. *J. Non-Newtonian Fluid Mech.* **166** (11), 546–553.

- BENZI, R., DE ANGELIS, E., GOVINDARAJAN, R. & PROCACCIA, I. 2003 Shell model for drag reduction with polymer additives in homogeneous turbulence. *Phys. Rev. E* **68**, 016308.
- BERMAN, N.S. 1978 Drag reduction by polymers. *Annu. Rev. Fluid Mech.* **10** (1), 47–64.
- BERTI, S., BISTAGNINO, A., BOFFETTA, G., CELANI, A. & MUSACCHIO, S. 2008 Two-dimensional elastic turbulence. *Phys. Rev. E* **77**, 055306.
- BERTI, S. & BOFFETTA, G. 2010 Elastic waves and transition to elastic turbulence in a two-dimensional viscoelastic Kolmogorov flow. *Phys. Rev. E* **82**, 036314.
- BHATTACHARJEE, J.K. & THIRUMALAI, D. 1991 Drag reduction in turbulent flows by polymers. *Phys. Rev. Lett.* **67**, 196–199.
- CAI, W.-H., LI, F.-C. & ZHANG, H.-N. 2010 DNS study of decaying homogeneous isotropic turbulence with polymer additives. *J. Fluid Mech.* **665**, 334–356.
- CASCIOLA, C.M. & DE ANGELIS, E. 2007 Energy transfer in turbulent polymer solutions. *J. Fluid Mech.* **581**, 419–436.
- CHOUERI, G.H., LOPEZ, J.M. & HOF, B. 2018 Exceeding the asymptotic limit of polymer drag reduction. *Phys. Rev. Lett.* **120**, 124501.
- DAVIDSON, P. 2015 *Turbulence: An Introduction for Scientists and Engineers*. Oxford University Press.
- DE LILLO, F., BOFFETTA, G. & MUSACCHIO, S. 2012 Control of particle clustering in turbulence by polymer additives. *Phys. Rev. E* **85**, 036308.
- DE TOONDER, J.M.J., HULSEN, M.A., KUIKEN, G.D.C. & NIEUWSTADT, F.T.M. 1997 Drag reduction by polymer additives in a turbulent pipe flow: numerical and laboratory experiments. *J. Fluid Mech.* **337**, 193–231.
- VAN DOORN E., WHITE C.M. & SREENIVASAN K.R. 1999 The decay of grid turbulence in polymer and surfactant solutions. *Phys. Fluids* **11** (8), 2387–2393.
- DUBIEF, Y., TERRAPON, V.E. & HOF, B. 2023 Elasto-inertial turbulence. *Annu. Rev. Fluid Mech.* **55** (1), 675–705.
- DUBIEF, Y., TERRAPON, V.E. & SORIA, J. 2013 On the mechanism of elasto-inertial turbulence. *Phys. Fluids* **25** (11), 110817.
- ESCUDIER, M.P., PRESTI, F. & SMITH, S. 1999 Drag reduction in the turbulent pipe flow of polymers. *J. Non-Newtonian Fluid Mech.* **81** (3), 197–213.
- FOGGI ROTA G., AMOR C., LE CLAINCHE S. & ROSTI M.E. 2024 Unified view of elastic and elasto-inertial turbulence in channel flows at low and moderate Reynolds numbers. *Phys. Rev. Fluids* **9**, L122602.
- FRISCH, U. 1996 *Turbulence: The Legacy of A. N. Kolmogorov*. Cambridge University Press.
- GILLISSEN, J.J.J. 2008 Polymer flexibility and turbulent drag reduction. *Phys. Rev. E* **78**, 046311.
- GILLISSEN, J.J.J. 2021 Weakened energy cascade in elastoinertial turbulence. *Phys. Rev. E* **103**, 063108.
- GROISMAN, A. & STEINBERG, V. 1998 Elastic vs. inertial instability in a polymer solution flow. *Europhys. Lett.* **43** (2), 165.
- GROISMAN, A. & STEINBERG, V. 2000 Elastic turbulence in a polymer solution flow. *Nature* **405** (6782), 53–55.
- GROISMAN, A. & STEINBERG, V. 2001 Efficient mixing at low Reynolds numbers using polymer additives. *Nature* **410** (6831), 905–908.
- GROISMAN, A. & STEINBERG, V. 2004 Elastic turbulence in curvilinear flows of polymer solutions. *New J. Phys.* **6** (1), 29.
- GUPTA, A. & VINCENZI, D. 2019 Effect of polymer-stress diffusion in the numerical simulation of elastic turbulence. *J. Fluid Mech.* **870**, 405–418.
- HINCH, E.J. 1977 Mechanical models of dilute polymer solutions in strong flows. *Phys. Fluids* **20** (10), S22–S30.
- IZBASSAROV, D., ROSTI, M.E., ARDEKANI, M.N., SARABIAN, M., HORMOZI, S., BRANDT, L. & TAMMISOLA, O. 2018 Computational modeling of multiphase viscoelastic and elastoviscoplastic flows. *Int. J. Numer. Methods Fluids* **88** (12), 521–543.
- KALELKAR, C., GOVINDARAJAN, R. & PANDIT, R. 2005 Drag reduction by polymer additives in decaying turbulence. *Phys. Rev. E* **72**, 017301.
- KIM, J. & MOIN, P. 1985 Application of a fractional-step method to incompressible Navier–Stokes equations. *J. Comput. Phys.* **59** (2), 308–323.
- KOLMOGOROV, A.N. 1941 Dissipation of energy in the locally isotropic turbulence. *Dokl. Akad. Nauk. SSSR* **32**, 19–21.
- KOLMOGOROV, A.N. 1962 A refinement of previous hypotheses concerning the local structure of turbulence in a viscous incompressible fluid at high Reynolds number. *J. Fluid Mech.* **13** (1), 82–85.
- KUMAR, M., GUASTO, J.S. & ARDEKANI, A.M. 2023 Lagrangian stretching reveals stress topology in viscoelastic flows. *Proc. Natl Acad. Sci. USA* **120** (5), e2211347120.

- LARSON, R.G. 1992 Instabilities in viscoelastic flows. *Rheol. Acta* **31** (3), 213–263.
- LEWY, T. & KERSWELL, R. 2024 Revisiting 2d viscoelastic Kolmogorov flow: a centre-mode-driven transition. arXiv: 2410.07402.
- LI, D.-Y., ZHANG, H., CHENG, J.-P., LI, X.-B., LI, F.-C., QIAN, S. & JOO, S.W. 2017 Numerical simulation of heat transfer enhancement by elastic turbulence in a curvy channel. *Microfluid Nanofluid* **21** (2), 25.
- LUMLEY, J.L. 1973 Drag reduction in turbulent flow by polymer additives. *J. Polymer Sci.: Macromol. Rev.* **7** (1), 263–290.
- L'VOV, V.S., POMYALOV, A., PROCACCIA, I. & TIBERKEVICH, V. 2004 Drag reduction by polymers in wall bounded turbulence. *Phys. Rev. Lett.* **92**, 244503.
- MIN, T., YOO, J.Y. & CHOI, H. 2001 Effect of spatial discretization schemes on numerical solutions of viscoelastic fluid flows. *J. Non-Newtonian Fluid Mech.* **100** (1), 27–47.
- NGUYEN, M.Q., DELACHE, A., SIMOËNS, S., BOS, W.J.T. & EL HAJEM, M. 2016 Small scale dynamics of isotropic viscoelastic turbulence. *Phys. Rev. Fluids* **1**, 083301.
- PAN, L., MOROZOV, A., WAGNER, C. & ARRATIA, P.E. 2013 Nonlinear elastic instability in channel flows at low Reynolds numbers. *Phys. Rev. Lett.* **110**, 174502.
- PERLEKAR, P., MITRA, D. & PANDIT, R. 2006 Manifestations of drag reduction by polymer additives in decaying, homogeneous, isotropic turbulence. *Phys. Rev. Lett.* **97**, 264501.
- PERLEKAR, P., MITRA, D. & PANDIT, R. 2010 Direct numerical simulations of statistically steady, homogeneous, isotropic fluid turbulence with polymer additives. *Phys. Rev. E* **82**, 066313.
- PICARDO, J.R., SINGH, R., RAY, S.S. & VINCENZI, D. 2020 Dynamics of a long chain in turbulent flows: impact of vortices. *Phil. Trans. R. Soc. A: Math. Phys. Engng Sci.* **378** (2175), 20190405.
- PROCACCIA, I., L'VOV, V.S. & BENZI, R. 2008 *Colloquium* : Theory of drag reduction by polymers in wall-bounded turbulence. *Rev. Mod. Phys.* **80**, 225–247.
- PTASINSKI, P.K., BOERSMA, B.J., NIEUWSTADT, F.T.M., HULSEN, M.A., VAN DEN BRULE, B.H.A.A. & HUNT, J.C.R. 2003 Turbulent channel flow near maximum drag reduction: simulations, experiments and mechanisms. *J. Fluid Mech.* **490**, 251–291.
- PTASINSKI, P.K., NIEUWSTADT, F.T.M., VAN DEN BRULE, B.H.A.A. & HULSEN, M.A. 2001 Experiments in turbulent pipe flow with polymer additives at maximum drag reduction. *Flow Turbul. Combust.* **66** (2), 159–182.
- QIN, B. & ARRATIA, P.E. 2017 Characterizing elastic turbulence in channel flows at low Reynolds number. *Phys. Rev. Fluids* **2**, 083302.
- RAY, S.S. & VINCENZI, D. 2016 Elastic turbulence in a shell model of polymer solution. *Europhys. Lett.* **114** (4), 44001.
- ROSTI, M.E., PERLEKAR, P. & MITRA, D. 2023 Large is different: Nonmonotonic behavior of elastic range scaling in polymeric turbulence at large Reynolds and Deborah numbers. *Sci. Adv.* **9** (11), eadd3831.
- SAMANTA, D., DUBIEF, Y., HOLZNER, M., SCHÄFER, C., MOROZOV, A.N., WAGNER, C. & HOF, B. 2013 Elasto-inertial turbulence. *Proc. Natl Acad. Sci. USA* **110** (26), 10557–10562.
- SHAQFEH, E.S.G. 1996 Purely elastic instabilities in viscometric flows. *Annu. Rev. Fluid Mech.* **28** (1), 129–185.
- SINGH, R.K. 2024 Elasticity of fibres prefers the chaos of turbulence. arXiv:2406.06033
- SINGH, R.K., PERLEKAR, P., MITRA, D. & ROSTI, M.E. 2024 Intermittency in the not-so-smooth elastic turbulence. *Nat. Commun.* **15** (1), 4070.
- SOLIGO, G. & ROSTI, M.E. 2023 Non-Newtonian turbulent jets at low-Reynolds number. *Intl J. Multiphase Flow* **167**, 104546.
- SREENIVASAN, K.R. & WHITE, C.M. 2000 The onset of drag reduction by dilute polymer additives, and the maximum drag reduction asymptote. *J. Fluid Mech.* **409**, 149–164.
- SUGIYAMA, K., II, S., TAKEUCHI, S., TAKAGI, S. & MATSUMOTO, Y. 2011 A full Eulerian finite difference approach for solving fluid–structure coupling problems. *J. Comput. Phys.* **230** (3), 596–627.
- TABOR, M. & DE GENNES, P.G. 1986 A cascade theory of drag reduction. *Europhys. Lett.* **2** (7), 519.
- TOMS, B.A. 1949 Some observations on the flow of linear polymer solutions through straight tubes at large Reynolds numbers. In *Proc. 1st Intl Congr. Rheol.*, vol. 2, pp. 135–141.
- TOMS, B.A. 1977 On the early experiments on drag reduction by polymers. *Phys. Fluids* **20** (10), S3–S5.
- VALENTE, P.C., DA SILVA, C.B. & PINHO, F.T. 2016 Energy spectra in elasto-inertial turbulence. *Phys. Fluids* **28** (7), 075108.
- VINCENZI, D., JIN, S., BODENSCHATZ, E. & COLLINS, L.R. 2007 Stretching of polymers in isotropic turbulence: a statistical closure. *Phys. Rev. Lett.* **98**, 024503.
- VIRK, P.S. 1975 Drag reduction fundamentals. *AIChE J.* **21** (4), 625–656.
- WAGNER, C.E. & MCKINLEY, G.H. 2016 The importance of flow history in mixed shear and extensional flows. *J. Non-Newtonian Fluid Mech.* **233**, 133–145.

- WHITE, C.M. & MUNGAL, M.G. 2008 Mechanics and prediction of turbulent drag reduction with polymer additives. *Annu. Rev. Fluid Mech.* **40** (1), 235–256.
- XI, L. 2019 Turbulent drag reduction by polymer additives: fundamentals and recent advances. *Phys. Fluids* **31** (12), 121302.
- YANG, S.-Q. & DOU, G. 2010 Turbulent drag reduction with polymer additive in rough pipes. *J. Fluid Mech.* **642**, 279–294.
- ZHANG, W.-H., ZHANG, H.-N., LI, Y.-K., YU, B. & LI, F.-C. 2021*a* Role of elasto-inertial turbulence in viscoelastic drag-reducing turbulence. *Phys. Fluids* **33** (8), 081706.
- ZHANG, Y.-B., BODENSCHATZ, E., XU, H. & XI, H.-D. 2021*b* Experimental observation of the elastic range scaling in turbulent flow with polymer additives. *Sci. Adv.* **7** (14), eabd3525.